Determination of an Application for an Environmental Permit under the Environmental Permitting (England & Wales) Regulations 2010

Decision document recording our decision-making process

The Permit Number is: EPR/YP3039EX
The Applicant / Operator is: CoGen Limited

The Installation is located at: Hooton Park Sustainable

Energy Facility

Biossence Hooton Park

North Road Hooton Park

Eastham, Merseyside

CH65 1AJ

What this document is about

This is a decision document, which accompanies a permit.

It explains how we have considered the Applicant's Application, and why we have included the specific conditions in the permit we are issuing to the Applicant. It is our record of our decision-making process, to show how we have taken into account all relevant factors in reaching our position. Unless the document explains otherwise, we have accepted the Applicant's proposals.

We try to explain our decision as accurately, comprehensively and plainly as possible. Achieving all three objectives is not always easy, and we would welcome any feedback as to how we might improve our decision documents in future. A lot of technical terms and acronyms are inevitable in a document of this nature: we provide a glossary of acronyms near the front of the document, for ease of reference.

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Preliminary information and use of terms

We gave the application the reference number EPR/YP3039EX/A001. We refer to the application as "the **Application**" in this document in order to be consistent.

The number we have given to the permit is EPR/YP3039EX. We refer to the permit as "the **Permit**" in this document.

The Application was duly made on 11/08/14.

The Applicant was originally Biossence Hooton Limited however a change of operator application was received on 09/07/15 transferring the Application to CoGen Limited. We refer to CoGen Limited as "the **Applicant**" in this document. Where we are talking about what would happen after the Permit is granted, we call CoGen Limited "the **Operator**".

CoGen Limited's proposed facility is located at Hooton Park Sustainable Energy Facility.

We refer to this as "the Installation" in this document.

How this document is structured

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Glossary of acronyms used in this document

(Please note that this glossary is standard for our decision documents and therefore not all these acronyms are necessarily used in this document.)

AAD Ambient Air Directive

APC Air Pollution Control

BAT Best Available Technique(s)

BAT-AEL BAT Associated Emission Level

BREF BAT Reference Note

CEM Continuous emissions monitor

CFD Computerised fluid dynamics

CHP Combined heat and power

COMEAP Committee on the Medical Effects of Air Pollutants

CROW Countryside and rights of way Act 2000

CV Calorific value

CW Clinical waste

CWI Clinical waste incinerator

DAA Directly associated activity – Additional activities necessary to be carried out to allow

the principal activity to be carried out

DD Decision document

EAL Environmental assessment level

EIAD Environmental Impact Assessment Directive (85/337/EEC)

ELV Emission limit value

EMAS EU Eco Management and Audit Scheme

EMS Environmental Management System

EPR Environmental Permitting (England and Wales) Regulations 2010 (SI 2010 No. 675) as

amended

EQS Environmental quality standard

EU-EQS European Union Environmental Quality Standard

EWC European waste catalogue

FSA Food Standards Agency

GWP Global Warming Potential

HHRAP Human Health Risk Assessment Protocol

HMIP Her Majesty's Inspectorate of Pollution

HPA Health Protection Agency (now PHE – Public Health England)

HRA Human Rights Act 1998

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HW Hazardous waste

HWI Hazardous waste incinerator

IBA Incinerator Bottom Ash

IED Industrial Emissions Directive (2010/75/EU)

IPPCD Integrated Pollution Prevention and Control Directive (2008/1/EC) – now superseded

by IED

I-TEF Toxic Equivalent Factors set out in Annex VI Part 2 of IED

I-TEQ Toxic Equivalent Quotient calculated using I-TEF

LCPD Large Combustion Plant Directive (2001/80/EC) – now superseded by IED

LCV Lower calorific value – also termed net calorific value

LfD Landfill Directive (1999/31/EC)

LOI Loss on Ignition

MBT Mechanical biological treatment

MSW Municipal Solid Waste

MWI Municipal waste incinerator

NOx Oxides of nitrogen (NO plus NO₂ expressed as NO₂)

Opra Operator Performance Risk Appraisal

PAH Polycyclic aromatic hydrocarbons

PC Process Contribution

PCB Polychlorinated biphenyls

PEC Predicted Environmental Concentration

PHE Public Health England

POP(s) Persistent organic pollutant(s)

PPS Public participation statement

PR Public register

PXDD Poly-halogenated di-benzo-p-dioxins

PXB Poly-halogenated biphenyls

PXDF Poly-halogenated di-benzo furans

RGS Regulatory Guidance Series

RHI Renewable Heat Incentive

ROC Renewable Obligation Certificate

SAC Special Area of Conservation

SED Solvent Emissions Directive (1999/13/EC) – now superseded by IED

SCR Selective catalytic reduction

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SGN Sector guidance note

SNCR Selective non-catalytic reduction

SPA(s) Special Protection Area(s)

SRF Solid Recovered Fuel

SS Sewage sludge

SSSI(s) Site(s) of Special Scientific Interest

SWMA Specified waste management activity

TDI Tolerable daily intake

TEF Toxic Equivalent Factors

TGN Technical guidance note

TOC Total Organic Carbon

UHV Upper heating value –also termed gross calorific value

UN_ECE United Nations Environmental Commission for Europe

US EPA United States Environmental Protection Agency

WFD Waste Framework Directive (2008/98/EC)

WHO World Health Organisation

WID Waste Incineration Directive (2000/76/EC) – now superseded by IED

We have decided to grant the Permit to the Applicant. This will allow it to operate the Installation, subject to the conditions in the Permit.

We consider that, in reaching that decision, we have taken into account all relevant considerations and legal requirements and that the permit will ensure that a high level of protection is provided for the environment and human health.

This Application is to operate an installation which is subject principally to the Industrial Emissions Directive (IED).

The Permit contains many conditions taken from our standard Environmental Permit template including the relevant Annexes. We developed these conditions in consultation with industry, having regard to the legal requirements of the Environmental Permitting Regulations and other relevant legislation. This document does not therefore include an explanation for these standard conditions. Where they are included in the permit, we have considered the Application and accepted the details are sufficient and satisfactory to make the standard condition appropriate. This document does, however, provide an explanation of our use of "tailor-made" or installation-specific conditions, or where our Permit template provides two or more options.

2 How we reached our decision

2.1 Receipt of Application

The Application was duly made on 11/08/14. This means we considered it was in the correct form and contained sufficient information for us to begin our determination but not that it necessarily contained all the information we would need to complete that determination: see below.

The Applicant made no claim for commercial confidentiality. We have not received any information in relation to the Application that appears to be confidential in relation to any party.

A change of operator request was received on 09/07/15 allowing CoGen Limited to take over the operation of the Hooton Park Sustainable Energy Facility from Biossence Hooton Facilities Management Limited.

2.2 Consultation on the Application

We carried out consultation on the Application in accordance with the EPR, our statutory PPS and our own RGS Note 6 for Determinations involving Sites of High Public Interest. We consider that this process satisfies, and frequently goes beyond the requirements of the Aarhus Convention on Access to Information, Public Participation in Decision-Making and Access to Justice in Environmental Matters, which are directly incorporated into the IED, which

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applies to the Installation and the Application. We have also taken into account our obligations under the Local Democracy, Economic Development and Construction Act 2009 (particularly Section 23). This requires us, where we consider it appropriate, to take such steps as we consider appropriate to secure the involvement of representatives of interested persons in the exercise of our functions, by providing them with information, consulting them or involving them in any other way. In this case, our consultation already satisfies the Act's requirements.

We advertised the Application by a notice placed on our website, which contained all the information required by the IED, including telling people where and when they could see a copy of the Application.

We sent copies of the Application to the following bodies, which includes those with whom we have "Working Together Agreements":

- Public Health England (PHE)
- Wirral Metropolitan Borough Council (NHS) Director of Public Health
- Wirral Metropolitan Borough Council Planning Department
- Wirral Metropolitan Borough Council Environmental Protection Department
- Health and Safety Executive (HSE)
- Food Standards Agency (FSA)
- Sewerage Undertaker United Utilities

These are bodies whose expertise, democratic accountability and/or local knowledge make it appropriate for us to seek their views directly. Note under our Working Together Agreement with Natural England, we only inform Natural England of the results of our assessment of the impact of the installation on designated Habitats sites.

Further details along with a summary of consultation comments and our response to the representations we received can be found in Annex 4. We have taken all relevant representations into consideration in reaching our determination.

2.3 Requests for Further Information

Although we were able to consider the Application duly made, we did in fact need more information in order to determine it, and requested further information via email on 09/01/15. The operator provided the information via emails received on 14/01/15 and 19/01/15.

In addition to our information notices, we received additional information during the determination from the operator on 15/09/14 comprising revised air dispersion modelling files for a single stream plant.

We requested further information via a Schedule 5 notice on 27/03/15 (reissued 11/06/15 due to change in operator) with respect to the specification of the waste derived fuel and systems to minimise odour. The responses

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received dated 09/07/15 and 02/09/15 clarified that the fuel would be SRF produced to the CEN 15359: 2011 standard and provided further information with respect to waste acceptance procedures (document titled Environment Agency: Hooton Feedstock Quality Management Procedures).

We made a copy of this information available to the public in the same way as the responses to our information notices.

3 The legal framework

The Permit will be granted under Regulation 13 of the EPR. The Environmental Permitting regime is a legal vehicle which delivers most of the relevant legal requirements for activities falling within its scope. In particular, the regulated facility is:

- an installation and a waste incineration plant as described by the IED;
- an operation covered by the WFD, and
- Subject to aspects of other relevant legislation which also have to be addressed.

We address some of the major legal requirements directly where relevant in the body of this document. Other requirements are covered in a section towards the end of this document.

We consider that, in granting the Permit, it will ensure that the operation of the Installation complies with all relevant legal requirements and that a high level of protection will be delivered for the environment and human health.

We explain how we have addressed specific statutory requirements more fully in the rest of this document.

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4 The Installation

4.1 Description of the Installation and related issues

4.1.1 The permitted activities

The Installation is subject to the EPR because it carries out an activity listed in Part 1 of Schedule 1 to the EPR:

Section 5.1 Part A(1)(b) – incineration of non-hazardous waste in a
waste incineration plant or waste co-incineration plant with a capacity
exceeding 3 tonnes per hour.

The IED definition of "waste incineration plants" and "waste co-incineration plants" says that it includes:

"all incineration lines or co-incineration lines, waste reception, storage, on-site pre-treatment facilities, waste, fuel and air supply systems, boilers, facilities for the treatment of waste gases, on-site facilities for treatment or storage of residues and waste water, stacks, devices for controlling incineration or co-incineration operations, recording and monitoring incineration or co-incineration conditions."

Many activities which would normally be categorised as "directly associated activities" for EPR purposes (see below), such as air pollution control plant and the ash storage bunker, are therefore included in the listed activity description.

An installation may also comprise "directly associated activities", which at this Installation includes the generation of electricity using a steam turbine and a back up electricity generator for emergencies. These activities comprise one installation, because the incineration plant and the steam turbine are successive steps in an integrated activity.

Together, these listed and directly associated activities comprise the Installation.

4.1.2 The Site

The Hooten Park Sustainable Energy Facility is located at Ordnance Survey Grid Reference SJ 373 799, some 1.5 km to the south-east of the centre of Eastham. The site is in an industrial area on the eastern coast of the Wirral, between Eastham to the west and Ellesmere Port to the south east. The site is surrounded by oil storage tanks to the north and south and is adjacent to an oil refinery to the west. To the east of the site is the Manchester Ship Canal. The wider industrial area around the proposed site includes the Vauxhall car

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plant amongst other uses. A significant proportion of the wider industrial area is vacant.

The nearest settlements to the proposed development are at Eastham to the north, Hooton to the south-west, and Ellesmere Port to the south. The nearest residential properties are those on the eastern fringe of Eastham, approximately 1 km to the north-west of the site, and along Rivacre Road a minimum of 750 metres to the south-west. Properties on the northern edge of Ellesmere Port / Childer Thornton lie approximately 2km to the south.

There are two Habitats sites (Special Areas of Conservation, Special Protection Areas or Ramsar sites) within 10km of the installation, the River Mersey and the Dee Estuary.

There are no Sites of Special Scientific Interest within 2km of the installation.

There are four non-statutory local wildlife and conservation sites and within 2km of the installation.

The Applicant submitted a plan which we consider is satisfactory, showing the site of the Installation and its extent. A plan is included in Schedule 7 to the Permit, and the Operator is required to carry on the permitted activities within the site boundary.

Further information on the site is addressed below at 4.3.

4.1.3 What the Installation does

The Applicant has described the facility as Energy from Waste. Our view is that for the purposes of IED (in particular Chapter IV) and EPR, the installation is a waste incineration plant because:

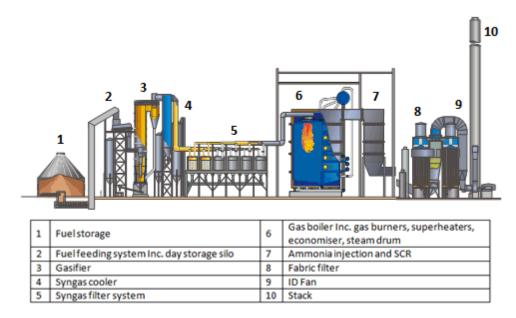
Notwithstanding the fact that energy will be recovered from the process; the process is never the less 'incineration' because it is considered that its main purpose is the thermal treatment of waste and

- The plant only produces electricity (and potentially heat in the future) but no material output:
- The waste is the principal source of fuel;
- The waste being burned is Solid Recovered Fuel (SRF) to the CEN 15359 2011 standard; and
- The waste has not been treated to improve its quality to a relevant standard.

The Installation will utilise circulating fluidised bed gasification technology with the capacity to burn approximately 266,000 tonnes per annum (34.1 tonnes per hour) of SRF, capable of generating up to 42 MWe using waste gasification technology.

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A process flow diagram is shown below with the relevant sections of the plant numbered for reference.



The facility is Combined Heat and Power (CHP) ready (8). If a district heating market becomes available, the provision of a heat off-take to supply a network would be possible without any modifications to the installed system.

The Installation includes the incoming fuel and screening, fuel storage, fuel feeding equipment, a gasifier, an ash removal system, a gasification air system, a starter burner and a product gas line including a cooler and filters, facilities for the treatment of exhaust gases, on-site facilities for treatment or storage of residues, devices and systems for controlling combustion operations, recording and monitoring conditions.

SRF is delivered to the Installation site via bulk loading trailers and screened and unloaded into the fuel storage silos (1) and transferred by conveyor (2) into the gasification day storage silos. The SRF is gasified in a circulating fluidised bed (3) to produce a product gas which is cooled in a gas cooler (4). Particulates are removed from the product gas by ceramic candles (5) and transferred off-site as a waste.

The cooled and filtered product gas is transferred to the burners in the boiler (6) for combustion. The boiler produces super-heated steam which is then passed to a steam turbine to generate electricity for export to the National Grid.

The flue gas treatment system (7) comprises selective catalytic reduction (SCR) for the reduction of oxides of nitrogen emissions, a bag house filter for the removal of particulates, the injection of lime to control acid gases and the injection of carbon (9), primarily to control dioxin emissions. The cleaned exhaust gases are released to atmosphere via an 80m stack (10).

Continuous monitoring of oxygen, carbon monoxide, hydrogen chloride, sulphur dioxide, nitrogen oxides, ammonia, volatile organic compounds and particulates is undertaken for the flue gases in the stack. Solid residues

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generated by the plant will be sampled on a regular basis to assess bottom ash burnout and to monitor the levels of specified pollutants.

Although the process used to thermally treat the waste is gasification; for the process not to be considered to be a waste incineration plant, the resultant gases from the gasification process must be purified to such an extent that they are no longer a waste prior to their combustion and can cause emissions no higher than those from the burning of natural gas. The Applicant has not demonstrated to our satisfaction that the gases have passed the 'end of waste' test as referred to in the Waste Framework Directive; therefore the whole process is considered to be a waste incineration plant and therefore subject to the requirements of Chapter IV of the IED.

The key features of the Installation can be summarised in the table below.

Waste throughput,	266,000/annum	34.1/hour	
Tonnes/line		- 11 1/1 10 d.	
Waste processed	SRF		
Number of lines	1		
Furnace technology	Gasification		
Auxiliary Fuel	Natural Gas		
Acid gas abatement	Semi-dry	Lime	
NOx abatement	SCR	Ammonia	
Reagent consumption	Natural Gas (Auxiliary Fuel): 392 te/annum		
	Ammonia (25% solution): 1,300 te/annum		
	Lime: 2,400 te/annum:		
	Limestone: 3,500 te		
	Activated carbon: 100 te/annum		
	Sand: 3,500 te/annum		
	Process water: 4 m ³ /hou	r	
Flue gas recirculation	No		
		Activated carbon	
Dioxin abatement			
	Grid Reference 337420, 3		
Dioxin abatement Stack	Grid Reference 337420, 3 Height, 80m	Diameter, 2.0 m	
Dioxin abatement	Grid Reference 337420, 3 Height, 80m Flow, 69.16 Nm ³ /s		
Dioxin abatement Stack	Grid Reference 337420, 3 Height, 80m Flow, 69.16 Nm ³ /s Temperature 135 °C	Diameter, 2.0 m	
Dioxin abatement Stack Flue gas Electricity generated	Grid Reference 337420, 3 Height, 80m Flow, 69.16 Nm³/s Temperature 135 °C 41.9 MWe	Diameter, 2.0 m Velocity, 22.83m/s 287,280 MWh	
Dioxin abatement Stack Flue gas Electricity generated Electricity exported	Grid Reference 337420, 3 Height, 80m Flow, 69.16 Nm ³ /s Temperature 135 °C	Diameter, 2.0 m Velocity, 22.83m/s	
Dioxin abatement Stack Flue gas Electricity generated	Grid Reference 337420, 3 Height, 80m Flow, 69.16 Nm³/s Temperature 135 °C 41.9 MWe	Diameter, 2.0 m Velocity, 22.83m/s 287,280 MWh	
Dioxin abatement Stack Flue gas Electricity generated Electricity exported	Grid Reference 337420, 3 Height, 80m Flow, 69.16 Nm³/s Temperature 135 °C 41.9 MWe 36.9 MWe Temperature, 537 °C Currently no opportunity h	Diameter, 2.0 m Velocity, 22.83m/s 287,280 MWh 252,998 MWh Pressure, 117 bar/MPa nowever If a district	
Dioxin abatement Stack Flue gas Electricity generated Electricity exported Steam conditions	Grid Reference 337420, 3 Height, 80m Flow, 69.16 Nm³/s Temperature 135 °C 41.9 MWe 36.9 MWe Temperature, 537 °C Currently no opportunity heating market becomes	Diameter, 2.0 m Velocity, 22.83m/s 287,280 MWh 252,998 MWh Pressure, 117 bar/MPa nowever If a district available, the provision of	
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4.1.4 Key Issues in the Determination

The key issues arising during this determination were the environmental impact of emissions to air from the Installation and assessing their potential effect on human health and the environment. The assessment includes habitats sites including non statutory sites within relevant distances from the installation. We therefore describe how we determined these issues in more detail in this document.

4.2 The site and its protection

4.2.1 Site setting, layout and history

The site is generally flat with a total area of approximately 7.5ha and is roughly rectangular in shape, oriented northwest to southeast along its long axis. Currently the site is generally open grassland and scrubland with some mature deciduous trees sparsely populated across the site and areas of denser vegetation around the perimeter. There is a densely wooded area located in the eastern corner and south of this area, within the site boundary, an area referred to as an Oil Storage Depot is located where the 'Recycling and Repairs Building' is proposed.

A Geotechnical and Geo-Environmental Desk Study commissioned by the operator reviewed existing data including an intrusive ground investigation study (2009) and concluded that the land contamination presented a low to moderate risk rating using a qualitative risk assessment procedure.

A review of the historical use of the land concluded that with some minor exceptions the land has largely remained untouched and undeveloped.

Geology

The report described the underlying geology as;

'Approximately two thirds of the Site, in the central, northern and western areas, is underlain by the red sandstone of the Wilmslow Sandstone Formation (formerly known as the Upper Mottled Sandstone) of the Sherwood Sandstone Group. The southeast third of the Site is underlain by red pebbly sandstone of the older Chester Pebble Beds Formation (formerly known as the Bunter Pebble Beds) of the Sherwood Sandstone Group. The two formations are separated by a normal extensional fault trending in a north – south direction, throwing to the west. The bedrock appears to be roughly subhorizontal across much of the area.'

Hydrology and Hydrogeology

No significant water bodies are present on site; there are a number of small, stagnant ponds and ditches within the southeast corner of the site. The nearest major water courses are the Manchester Ship Canal and River Mersey, 80m and 150m northeast of the site respectively.

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4.2.2 <u>Proposed site design: potentially polluting substances and prevention</u> measures

The loading and unloading of vehicles will take place in designated areas which will have an impermeable hard surface designed to connect to the process water drainage system.

The facilities will be designed to comply with Environment Agency Guidelines as detailed below:

PPG1 - General Guide to the Prevention of Pollution

PPG 2 - Above Ground Oil Storage Tanks;

PPG 18 - Managing fire water and major spillages;

PPG 21 - Incident Response Planning; and

PPG 22 - Dealing with spills.

The solid materials on site (SRF, Limestone, activated carbon, air pollution control residues and filter ash) will be stored in silos surrounded by concrete hardstanding. The silos will have high level alarms and vent to atmosphere via a fabric filter. The filter will be cleaned with compressed air after filling operations. Bottom ash from the fluidised bed will be sieved and the sand fraction returned to the bed the residue will be stored in ash containers/vessels.

The 25% ammonia solution and boiler treatment chemicals will be stored in tanks bunded to 110% of their capacity surrounded by concrete hardstanding.

Ancillary materials such as hydraulic oils, glycol etc will be handled and stored in accordance with the Control of Substances Hazardous to Health Regulations (COSHH).

Suitable equipment to clean up any spillages will be provided and maintained.

Given the materials used within the activities of the Installation, the management and physical measures available and the sensitivity of the land on which the site is located, we consider that the likelihood of incidents involving loss of containment is low and the overall risk to the environment is not significant. We also consider that the provisions for contaminated fire water retention are sufficient to meet the requirements of IED Article 46(5). We are therefore satisfied that the ground and groundwater can be protected from the activities of this Installation.

However, at the time of application the specific detail and final arrangements of the drainage system was not able to be totally confirmed, we have therefore included pre-operational condition P06 which requires the operator to provide a detailed as-installed site drainage plan and the specific design detail of the site containment infrastructure, including all sub-surface structures and equipment. This condition also requires that a specific inspection and maintenance programme is to be provided for the site containment infrastructure, so that the 'lifetime' sections of the SCR can be implemented from the commencement of operations at the site.

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Article 22(2) of the IED the Applicant is required to provide a baseline report containing at least the information set out in paragraphs (a) and (b) of the Article before starting operation.

The Applicant has submitted a site condition report which includes a report on the baseline conditions as required by Article 22. We have reviewed that report and consider that it adequately describes the condition of the soil and groundwater prior to the start of operations. However the Applicant has confirmed that prior to construction the site will be cleared and if any contamination is identified samples will be taken and records kept.

The baseline report is an important reference document in the assessment of contamination that might arise during the operational lifetime of the installation and at cessation of activities at the installation.

4.2.3 Closure and decommissioning

Having considered the information submitted in the Application, we are satisfied that the appropriate measures will be in place for the closure and decommissioning of the Installation, as referred to in section 2.9 of the Application. Pre-operational condition PO1 requires the Operator to have an Environmental Management System in place before the Installation is operational, and this will include a site closure plan.

At the definitive cessation of activities, the Operator has to satisfy us that the necessary measures have been taken so that the site ceases to pose a risk to soil or groundwater, taking into account both the baseline conditions and the site's current or approved future use. To do this, the Operator has to apply to us for surrender, which we will not grant unless and until we are satisfied that these requirements have been met.

4.3 Operation of the Installation – general issues

4.3.1 Administrative issues

The Applicant is the sole Operator of the Installation.

We are satisfied that the Applicant is the person who will have control over the operation of the Installation after the granting of the Permit; and that the Applicant will be able to operate the Installation so as to comply with the conditions included in the Permit.

The incineration of waste is not a specified waste management activity (SWMA). The Environment Agency has considered whether any of the other activities taking place at the Installation are SWMAs and is satisfied that none are taking place.

We are satisfied that the Applicant's submitted Opra profile is accurate.

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The Opra score will be used as the basis for subsistence and other charging, in accordance with our Charging Scheme. Opra is the Environment Agency's method of ensuring application and subsistence fees are appropriate and proportionate for the level of regulation required.

4.3.2 Management

The Applicant has stated in the Application that they will implement an Environmental Management System (EMS) that will be certified under ISO14001. A pre-operational condition (PO1) is included requiring the Operator to provide a summary of the EMS prior to commissioning of the plant and to make available for inspection all EMS documentation. The Environment Agency recognises that certification of the EMS cannot take place until the Installation is operational. An improvement condition (IC1) is included requiring the Operator to report progress towards gaining certification of its EMS.

We are satisfied that appropriate management systems and management structures will be in place for this Installation, and that sufficient resources are available to the Operator to ensure compliance with all the Permit conditions.

4.3.3 Site security

Having considered the information submitted in the Application, we are satisfied that appropriate infrastructure and procedures will be in place to ensure that the site remains secure.

4.3.4 Accident management

The Applicant has not submitted a comprehensive Accident Management Plan. However, having considered the Plan and other information submitted in the Application, we are satisfied that appropriate measures will be in place to ensure that accidents that may cause pollution are prevented but that, if they should occur, their consequences are minimised. An Accident Management Plan will form part of the Environmental Management System and must be in place prior to commissioning as required by a pre-operational condition (PO1).

4.3.5 Off-site conditions

We do not consider that any off-site conditions are necessary.

4.3.6 Operating techniques

We have specified that the Applicant must operate the Installation in accordance with the following documents contained in the Application:

Description	Parts Included	Justification
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The Application	Parts B2 and B3 of the Application Form. The Supporting Information document including its associated Annex sections.	Together these sections describe key operating techniques and how the Installation will be operated to ensure that best available techniques are applied.
Additional Information Received 15/09/14	Email	
Additional Information Received 14/01/15	Email	Further information regarding plant operational conditions and natural gas usage.
Additional Information Received 19/01/15	Email	Supporting information addressing compliance with Articles 47, 50(2), 50(3) and 50(4) of IED.

The details set out above describe the techniques that will be used for the operation of the Installation that have been assessed by the Environment Agency as BAT; they form part of the Permit through Permit condition 2.3.1 and Table S1.2 in the Permit Schedules.

We have also specified the following limits and controls on the use of raw materials and fuels:

Raw Material or Fuel	Specifications	Justification
Gas Oil for back up	< 0.1% sulphur content	As required by Sulphur
generators		Content of Liquid Fuels
		Regulations.

Article 45(1) of the IED requires that the Permit must include a list of all types of waste which may be treated using at least the types of waste set out in the European Waste List established by Decision 2005/532/EC, EC, if possible, and containing information on the quantity of each type of waste, where appropriate. The Application contains a list of those wastes coded by the European Waste Catalogue (EWC) number, which the Applicant will accept in the waste streams entering the plant and which the plant is capable of burning in an environmentally acceptable way. We have specified the permitted waste types, descriptions and where appropriate quantities which can be accepted at the installation in Table S2.2.

We are satisfied that the Applicant can accept the wastes contained in Table S2.2 of the Permit because: -

these wastes are categorised as Wastes from Waste Management Facilities (Combustible waste (refuse derived fuel)) in the European Waste Catalogue;

(i) the wastes are all categorised as non-hazardous in the European Waste Catalogue and are capable of being safely burnt at the installation.

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- (ii) these wastes are likely to be within the design calorific value (CV) range for the plant;
- (iii) these wastes are unlikely to contain harmful components that cannot be safely processed at the Installation.

The incineration plant will take SRF. Waste codes for separately collected fractions of waste (with the exception of waste wood classified under EWC code 20 01 38) are not included in the list of permitted wastes, except that separately collected fractions which prove to be unsuitable for recovery may be included.

We have included pre-operational condition P04 that requires the Applicant to submit a report that details the waste acceptance procedure to be used at the site. This procedure will need to include the process and systems by which wastes unsuitable for incineration at the site will be controlled.

We have limited the capacity of the Installation to 266,000 tonnes per annum. This is based on the installation operating 7,800 hours per year at a nominal capacity of 34.1 tonnes per hour.

The Installation will be designed, constructed and operated using BAT for the incineration of the permitted wastes. We are satisfied that the operating and abatement techniques are BAT for incinerating these types of waste. Our assessment of BAT is set out later in this document.

4.3.7 Energy efficiency

(i) Consideration of energy efficiency

We have considered the issue of energy efficiency in the following ways:

- 1. The use of energy within, and generated by, the Installation which are normal aspects of all EPR permit determinations. This issue is dealt with in this section.
- 2. The extent to which the Installation meets the requirements of Article 50(5) of the IED, which requires "the heat generated during the incineration and co-incineration process is recovered as far as practicable through the generation of heat, steam or power". This issue is covered in this section.
- 3. The combustion efficiency and energy utilisation of different design options for the Installation are relevant considerations in the determination of BAT for the Installation, including the Global Warming Potential of the different options. This aspect is covered in the BAT assessment in section 6 of this Decision Document.

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(ii) Use of energy within the Installation

Having considered the information submitted in the Application, we are satisfied that appropriate measures will be in place to ensure that energy is used efficiently within the Installation.

The Application details a number of measures that will be implemented at the Installation in order to increase its energy efficiency.

The Application states that the specific energy consumption, a measure of total energy consumed per unit of waste processed, will be 146.6 kWh/tonne. The installation capacity is 266,000 t/a.

Data from the BREF for Municipal Waste Incinerators shows that the range of specific energy consumptions is as in the table below.

MSWI plant size range (t/yr)	Process energy demand (kWh/t waste input)
Up to 150,000	300 – 700
150,000 - 250,000	150 – 500
More than 250,000	60 – 200

The BREF says that it is BAT to reduce the average installation electrical demand to generally below 150 kWh/tonne of waste with an LCV of 10.4 MJ/kg. The LCV in this case is expected to be 13 MJ/kg which is high due to the waste being SRF. The specific energy consumption in the Application is in line with that set out above.

(iii) <u>Generation of energy within the Installation - Compliance with Article</u> 50(5) of the IED

Article 50(5) of the IED requires that "the heat generated during the incineration and co-incineration process is recovered as far as practicable".

Our CHP Ready Guidance (February 2013) considers that BAT for energy efficiency for Energy from Waste (EfW) plant is the use of CHP in circumstances where there are technically and economically viable opportunities for the supply of heat from the outset.

The term CHP in this context represents a plant which also provides a supply of heat from the electrical power generation process to either a district heating network or to an industrial / commercial building or process. However, it is recognised that opportunities for the supply of heat do not always exist from the outset (i.e. when a plant is first consented, constructed and commissioned).

In cases where there are no immediate opportunities for the supply of heat from the outset, the Environment Agency considers that BAT is to build the plant to be CHP Ready (CHP-R) to a degree which is dictated by the likely future opportunities which are technically viable and which may, in time, also become economically viable.

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The BREF says that where a plant generates electricity only, it is BAT to recover 0.4-0.65 MWh/ tonne of waste (based on LCV of 10.4 MJ/kg) for raw waste inputs or 0.6-1.0 MWh/tonne of waste (based on LCV of 15.2 MJ/kg) for pre-treated wastes. Our technical guidance note, SGN EPR S5.01, states that where electricity only is generated, 5-9 MW of electricity should be recoverable per 100,000 tonnes/annum of waste (which equates to 0.4-0.72 MWh/tonne of waste).

The Installation will generate electricity only and has been specified to maximise electrical output with little or no use of waste heat. The Sankey diagram in section 2.6.2 of the Application shows 41.9 MW of electricity produced for an annual burn of 266,000 tonnes, which represents 15.8 MW per 100,000 tonnes/yr of waste burned (1.08 MWh/tonne of waste). The Installation is therefore above the indicative BAT range due to the high SRF fuel % of the waste fuel input.

The SGN and Chapter IV of the IED both require that, as well as maximising the primary use of heat to generate electricity; waste heat should be recovered as far as practicable.

The location of the Installation largely determines the extent to which waste heat can be utilised, and this is a matter for the planning authority. The Applicant carried out a feasibility study, which showed there was potential to provide district heating to local businesses; suitable opportunities are being explored, though there are no firm commitments at this stage. There is provision within the design of the steam turbine to extract low-grade steam for a district heating scheme. Establishing a district heating network to supply local users would involve significant technical, financial and planning challenges such that this is not seen as a practicable proposition at present.

We consider that, within the constraints of the location of the Installation explained above, the Installation will recover heat as far as practicable, and therefore that the requirements of Article 6(6) are met.

(iv) R1 Calculation and the DEFRA Good Quality CHP Scheme

The R1 calculation and / or gaining accreditation under the DEFRA Good Quality CHP Scheme does not form part of the matters relevant to our determination. They are however general indicators that the installation is achieving a high level of energy recovery.

The Applicant has not presented an R1 calculation with this application, nor have we received a separate application for a determination on whether the installation is a recovery or disposal facility.

Note that the availability or non-availability of financial incentives for renewable energy such as the ROC and RHI schemes is not a consideration in determining this application.

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(v) Choice of Steam Turbine

The turbine generator arrangement will generate electrical power for export to the local electricity distribution network. The turbine facility will be 'CHP-Ready' with capability to export heat to local heat users. District heating schemes typically operate with a flow temperature of 90°C to 120°C and return water temperatures of 50°C to 80°C. Steam is extracted from the turbine at low pressure to maximise the power generated from the steam. To facilitate this, the turbine will be equipped with steam extraction points to allow low pressure steam to be supplied directly to heat users, or to be condensed in heat exchangers in order to provide hot water.

(vi) Choice of Cooling System

Wet steam emerges from the steam turbine typically at around 40°C. The steam holds approximately two thirds of the energy from the steam. This energy can be recovered in the form of low grade hot water from the condenser depending on the type of cooling implemented. Installing a mechanical draught or hybrid cooling tower would allow the heat recovered by the cooling water to be used for heating instead of being rejected in the cooling tower. This does not reduce the power output from the plant. However the heat is very low grade and there are few viable uses for the heat. Typically under-floor heating uses hot water of 40°C; however under floor heating is likely only to be economically viable in new build developments where conventional wet type radiator systems are more common in the UK.

An air-cooled condenser will be installed at this facility. Steam is condensed in a large air cooled system which rejects the heat in the steam into the air flow. An air cooled condenser does generate a similar temperature condensate, but cooling this condensate further by using it for space heating requires more steam to be extracted from the turbine to heat the feedwater prior to being pumped into the boiler. The additional steam extraction reduces the power generation from the plant.

(vii) Permit conditions concerning energy efficiency

Pre-operational condition PO1 requires the Operator to carry out a comprehensive review of the available heat recovery options prior to commissioning, in order to ensure that waste heat from the plant is recovered as far as possible.

Conditions 1.2.2 and 1.2.3 have also been included in the Permit, which require the Operator to review the options available for heat recovery on an ongoing basis, and to provide and maintain the proposed steam/hot water pass-outs.

The Operator is required to report energy usage and energy generated under condition 4.2 and Schedule 5. The following parameters are required to be reported: total electrical energy generated; electrical energy exported; total

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energy usage and energy exported as heat (if any). Together with the total MSW burned per year, this will enable the Environment Agency to monitor energy recovery efficiency at the Installation and take action if at any stage the energy recovery efficiency is less than proposed.

There are no site-specific considerations that require the imposition of standards beyond indicative BAT, and so the Environment Agency accepts that the Applicant's proposals represent BAT for this Installation.

4.3.8 Efficient use of raw materials

Having considered the information submitted in the Application, we are satisfied that the appropriate measures will be in place to ensure the efficient use of raw materials and water.

The Operator is required to report with respect to raw material usage under condition 4.2. and Schedule 5, including consumption of lime, limestone, activated carbon and ammonia used per tonne of waste burned. This will enable the Environment Agency to assess whether there have been any changes in the efficiency of the air pollution control plant, and the operation of the SCR to abate NO_x . These are the most significant raw materials that will be used at the Installation, other than the waste feed itself (addressed elsewhere). The efficiency of the use of auxiliary fuel will be tracked separately as part of the energy reporting requirement under condition 4.2.1. Optimising reagent dosage for air abatement systems and minimising the use of auxiliary fuels is further considered in the section on BAT.

4.3.9 <u>Avoidance, recovery or disposal with minimal environmental impact of wastes produced by the activities</u>

This requirement addresses wastes produced at the Installation and does not apply to the waste being treated there. The principal waste streams the Installation will produce are bottom ash, air pollution control residues, syngas filtration residues and recovered metals.

The first objective is to avoid producing waste at all. Waste production will be avoided by achieving a high degree of burnout of the ash in the furnace, which results in a material that is both reduced in volume and in chemical reactivity. Condition 3.5.1 and associated Table S3.5 specify limits for total organic carbon (TOC) of <3% in bottom ash. Compliance with this limit will demonstrate that good combustion control and waste burnout is being achieved in the furnaces and waste generation is being avoided where practicable.

Incinerator bottom ash (IBA) will normally be classified as non-hazardous waste. However, IBA is classified on the European List of Wastes as a "mirror entry", which means IBA is a hazardous waste if it possesses a hazardous property relating to the content of dangerous substances. Monitoring of incinerator ash will be carried out in accordance with the requirements of

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Article 53(3) of IED. Classification of IBA for its subsequent use or disposal is controlled by other legislation and so is not duplicated within the permit.

Air pollution control (APC) residues and syngas filtration residues (SFR) from flue gas treatment are hazardous waste and therefore must be sent for disposal to a landfill site permitted to accept hazardous waste, or to an appropriately permitted facility for hazardous waste treatment. The amount of residues is minimised through optimising the performance of the syngas filtration system and air emissions abatement plant.

In order to ensure that the IBA, SFR and APC residues are adequately characterised, pre-operational condition PO2 requires the Operator to provide a written plan for approval detailing the ash sampling protocols. Table S3.5 requires the Operator to carry out an ongoing programme of monitoring.

The Application states that the syngas is cooled by a gas cooler to 350-450°C to convert alkalis and heavy metals into solids and sent for disposal. The Application also proposes that, where possible, bottom ash will be transported to a suitable recycling facility, from where it could be re-used in the construction industry as an aggregate. The Applicant is currently investigating options for the use of bottom ash in road construction.

Having considered the information submitted in the Application, we are satisfied that the waste hierarchy referred to in Article 4 of the WFD will be applied to the generation of waste and that any waste generated will be treated in accordance with this Article.

We are satisfied that waste from the Installation that cannot be recovered will be disposed of using a method that minimises any impact on the environment. Standard condition 1.4.1 will ensure that this position is maintained.

5. Minimising the Installation's environmental impact

Regulated activities can present different types of risk to the environment, these include odour, noise and vibration; accidents, fugitive emissions to air and water; as well as point source releases to air, discharges to ground or groundwater, global warming potential and generation of waste and other environmental impacts. Consideration may also have to be given to the effect of emissions being subsequently deposited onto land (where there are ecological receptors). All these factors are discussed in this and other sections of this document.

For an installation of this kind, the principal emissions are those to air, although we also consider those to land and water.

The next sections of this document explain how we have approached the critical issue of assessing the likely impact of the emissions to air from the

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Installation on human health and the environment and what measures we are requiring to ensure a high level of protection.

5.1 <u>Assessment Methodology</u>

5.1.1 Application of Environment Agency H1 Guidance

A methodology for risk assessment of point source emissions to air, which we use to assess the risk of applications we receive for permits, is set out in our Horizontal Guidance Note H1 and has the following steps:

- Describe emissions and receptors
- Calculate process contributions
- Screen out insignificant emissions that do not warrant further investigation
- Decide if detailed air modelling is needed
- Assess emissions against relevant standards
- Summarise the effects of your emissions

The H1 methodology uses a concept of "process contribution (PC)", which is the estimated concentration of emitted substances after dispersion into the receiving environmental media at the point where the magnitude of the concentration is greatest. The guidance provides a simple method of calculating PC primarily for screening purposes and for estimating process contributions where environmental consequences are relatively low. It is based on using dispersion factors. These factors assume worst case dispersion conditions with no allowance made for thermal or momentum plume rise and so the process contributions calculated are likely to be an overestimate of the actual maximum concentrations. More accurate calculation of process contributions can be achieved by mathematical dispersion models, which take into account relevant parameters of the release and surrounding conditions, including local meteorology – these techniques are expensive but normally lead to a lower prediction of PC.

5.1.2 <u>Use of Air Dispersion Modelling</u>

For incineration applications, we normally require the Applicant to submit a full air dispersion model as part of their application. Air dispersion modelling enables the process contribution to be predicted at any environmental receptor that might be impacted by the plant.

Once short-term and long-term PCs have been calculated in this way, they are compared with Environmental Quality Standards (EQS) referred to as "benchmarks" in the H1 Guidance.

Where an EU EQS exists, the relevant standard is the EU EQS. Where an EU EQS does not exist, our guidance sets out a National EQS (also referred to as Environmental Assessment Level - EAL) which has been derived to provide a similar level of protection to Human Health and the Environment as the EU EQS levels. In a very small number of cases, e.g. for emissions of Lead, the

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National EQS is more stringent that the EU EQS. In such cases, we use the National EQS standard for our assessment.

National EQSs do not have the same legal status as EU EQSs, and there is no explicit requirement to impose stricter conditions than BAT in order to comply with a national EQS. However, national EQSs are a standard for harm and any significant contribution to a breach is likely to be unacceptable.

PCs are considered **Insignificant** if:

- the **long-term** process contribution is less than **1%** of the relevant EQS; and
- the **short-term** process contribution is less than **10**% of the relevant EQS.

The **long term** 1% process contribution insignificance threshold is based on the judgements that:

- It is unlikely that an emission at this level will make a significant contribution to air quality;
- The threshold provides a substantial safety margin to protect health and the environment.

The **short term** 10% process contribution insignificance threshold is based on the judgements that:

- spatial and temporal conditions mean that short term process contributions are transient and limited in comparison with long term process contributions;
- the proposed threshold provides a substantial safety margin to protect health and the environment.

Where an emission is screened out in this way, we would normally consider that the Applicant's proposals for the prevention and control of the emission to be BAT. That is because if the impact of the emission is already insignificant, it follows that any further reduction in this emission will also be insignificant.

However, where an emission cannot be screened out as insignificant, it does not mean it will necessarily be significant.

For those pollutants which do not screen out as insignificant, we determine whether exceedences of the relevant EQS are likely. This is done through detailed audit and review of the Applicant's air dispersion modelling taking background concentrations and modelling uncertainties into account. Where an excedance of an EU EQS is identified, we may require the Applicant to go beyond what would normally be considered BAT for the Installation or we may refuse the application if the applicant is unable to provide suitable alternative proposals. Whether or not exceedences are considered likely, the application is subject to the requirement to operate in accordance with BAT.

This is not the end of the risk assessment, because we also take into account local factors (for example, particularly sensitive receptors nearby such as a

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SSSIs, SACs or SPAs). These additional factors may also lead us to include more stringent conditions than BAT.

If, as a result of reviewing of the risk assessment and taking account of any additional techniques that could be applied to limit emissions, we consider that emissions **would cause significant pollution**, we would refuse the Application.

5.2 Assessment of Impact on Air Quality

The Applicant's assessment of the impact of air quality is set out in the Biossence Air Quality Assessment (issue 2 - 01/07/2014) and supporting documents of the Application. The assessment comprises:

- An H1 screening assessment of emissions to air from the operation of the incinerator.
- Dispersion modelling of emissions to air from the operation of the incinerator.
- A study of the impact of emissions on nearby sensitive habitat / conservation sites.

Amenity impacts during construction and air quality impacts arising from additional road traffic have not been considered as these are essentially matters for the local planning authority when considering the parallel application for planning permission, and outside the scope of our determination under the Environmental Permitting Regulations.

This section of the decision document deals primarily with the dispersion modelling of emissions to air from the incinerator chimney and its impact on local air quality. The impact on conservation sites is considered in section 5.4 and odour impacts are considered in section 5.6.

The Applicant has assessed the Installation's potential emissions to air against the relevant air quality standards, and the potential impact upon local conservation and habitat sites and human health. These assessments predict the potential effects on local air quality from the Installation's stack emissions using the ADMS 5 dispersion model, which is a commonly used computer model for regulatory dispersion modelling. The model used 5 years of meteorological data collected from the weather station at Liverpool Speke between 2008 and 2011 which is the closest station to the site at 7.4km. The impact of the terrain surrounding the site upon plume dispersion was not considered in the dispersion modelling. Following a review by our Air Quality specialists of the model domain on our mapping systems we agree with this approach.

The air impact assessments, and the dispersion modelling upon which they were based, employed the following assumptions.

- First, they assumed that the ELVs in the Permit with the exception of Oxides of nitrogen (NO_x) would be the maximum permitted by Article 46(2) of the IED. These substances are:
 - Total dust

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- Carbon monoxide (CO)
- Sulphur dioxide (SO₂)
- Hydrogen chloride (HCl)
- Hydrogen fluoride (HF)
- Metals (Cadmium, Thallium, Mercury, Antimony, Arsenic, Lead, Chromium, Cobalt, Copper, Manganese, Nickel and Vanadium)
- Polychlorinated dibenzo-para-dioxins and polychlorinated dibenzo furans (referred to as dioxins and furans)
- Gaseous and vaporous organic substances, expressed as Total Organic Carbon (TOC)
- Oxides of nitrogen (NO_x), expressed as NO₂ are assumed to be half the maximum permitted by Article 46(2) of the IED as the use of selective catalytic conversion (SCR) enables this to be achieved.
- Second, they assumed that the Installation operates continuously at the relevant long-term or short-term emission limit values, i.e. the maximum permitted emission rate.
- Third, the model also considered emissions of pollutants not covered by Annex VI of IED, specifically ammonia (NH₃), nitrous oxide (N₂O) Polycyclic Aromatic Hydrocarbons (PAH) and PCB's. Emission rates used in the modelling have been drawn from data in the Waste Incineration BREF and are considered further in section 5.2.5.

We are in agreement with this approach. The assumptions underpinning the model have been checked and are reasonably precautionary.

The Applicant has utilised modelled background concentrations provided by DEFRA (on a 1 Km by 1 Km grid) to augment the data available from local authority monitoring. This data is summarised in the Application and has been used by the Applicant to establish the background (or existing) air quality against which to measure the potential impact of the incinerator.

As well as calculating the peak ground level concentration, the Applicant has modelled the concentration of key pollutants at a number of specified locations within the surrounding area.

The way in which the Applicant used dispersion models, its selection of input data, use of background data and the assumptions it made have been reviewed by the Environment Agency's modelling specialists to establish the robustness of the Applicant's air impact assessment. The output from the model has then been used to inform further assessment of health impacts and impact on habitats and conservation sites.

Our review of the Applicant's assessment leads us to agree with the Applicant's conclusions. We have also audited the air quality and human health impact assessment and similarly agree that the conclusions drawn in the reports were acceptable.

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The Applicant's modelling predictions are summarised in the following sections.

5.2.1 <u>Assessment of Air Dispersion Modelling Outputs</u>

The Applicant's modelling predictions are summarised in the tables below. The figures shown indicate the predicted peak ground level exposure to pollutants in ambient air. Whilst we have used the Applicant's modelling predictions in the table below, we have made our own simple verification calculation of the percentage process contribution and predicted environmental concentration. These are the numbers shown in the tables below and so may be very slightly different to those shown in the Application. Any such minor discrepancies do not materially impact on our conclusions.

Assessment of Emissions to Air (1)

Pollutant	EQS/E	AL	Back- ground	Process Co (PC)	ontribution	Predicted Environme Concentra	
	μg/m³		μg/m³	μg/m³	% of EAL	μg/m³	% of EAL
NO ₂	40	1	29.74	0.48	1.20	30.2	75.6
	200	2	59.48	4.23	2.1	63.71	31.9
PM ₁₀	40	1	16.73	0.07	0.18	16.8	42.0
	50	3	33.46	0.23	0.46	33.69	67.4
PM _{2.5}	25	1	11.99	0.02	0.08	12.01	48.0
SO ₂	266	4	22.6	7.13	2.7	29.73	11.2
	350	5	22.6	5.79	1.65	28.39	4.9
	125	6	22.6	2.88	2.3	25.48	20.4
HCI	750	7	1.06	2.68	0.36	3.7	0.5
HF	16	8	2.35	0.01	0.06	2.36	14.75
	160	7	4.7	0.27	0.17	4.97	3.1
СО	10000	9	760	6.5	0.06	766	7.7
TOC	2.25	1	0.14	0.07	3.11	0.21	9.33
PAH	0.00025	1	0.00026	0.0000014	0.56	0.000261	104.6
NH ₃	180	1	2.33	0.07	0.04	2.4	1.33
	2500	10	4.66	2.68	0.11	7.34	0.3
PCBs	0.2	1	0.00026	0.00003	0.02	0.00029	0.15
	6	10	0.00052	0.0013	0.02	0.00182	0.03
Dioxins			3.9E-08	6.80E-10		3.97E-08	

TOC as 1,3 butadiene, PAH as benzo[a]pyrene

- 1 Annual Mean
- 2 99.79th %ile of 1-hour mean
- 3 90.41st %ile of 24-hour mean
- 4 99.9th ile of 15-min mean
- 5 99.73rd %ile of 1-hour mean
- 6 99.18th %ile of 24-hour mean
- 7 1-hour average
- 8 Monthly average
- 9 Maximum daily running 8-hour mean
- 10 1-hour maximum

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Assessment of Emissions to Air (2)

Pollutant	EQS / EAL		Back- ground	Process Contributi	ion	Predicted Environme Concentra	
	μg/m³		μg/m³	μg/m³	% of EAL	μg/m³	% of EAL
Cd TI	0.005	1	0.00016	0.00034	6.8	0.00050 0	10.0
Hg	0.25 7.5	1 2	0.0233 0.0466	0.00034 0.0134	0.14 0.18	0.02364 0.06000	9.46 0.800
Sb	5 150	1 2		0.0034 0.134	0.07 0.09	0.0034 0.13400	0.07 0.089
Pb Co	0.25	1	0.0042 0.00034	0.0034 0.0034	1.36	0.00760 0.00374	3.04
Cu	10 200	1 2	0.00742 0.01484	0.0034 0.134	0.03 0.07	0.01082 0.14884	0.108 0.074
Mn	0.15 1500	1 2	0.00979 0.01958	0.0034 0.134	2.27 0.01	0.01319 0.15358	8.79 0.0102
V	5	1 3	0.00147 0.00294	0.0034 0.134	0.07 13.40	0.00487 0.13694	0.10 13.69
As	0.003	1	0.00074	0.0034	113.33	0.00414	138.0
Cr (II)(III)	5 150	1 2	0.00248 0.00496	0.0034 0.134	0.07 0.09	0.00588 0.13896	0.118 0.0926
Cr (VI) Ni	0.0002 0.02	1 1	0.00050 0.00142	0.0034 0.0034	1700.00 17.00	0.00390 0.00482	1950.0 24.1

- 1 Annual Mean
- 2 1-hr Maximum
- 3 24-hr Maximum

(i) Screening out emissions which are insignificant

From the tables above the following emissions can be screened out as insignificant in that the process contribution is < 1% of the long term EQS/EAL and <10% of the short term EAQ/EAL. These are:

• PM₁₀, PM_{2.5}, SO₂, HCl, HF, CO, PAH, NH₃, PCBs, Dioxins, Hg, Sb, Co, Cu and Cr (II) (III).

Therefore, generally, we consider the Applicant's proposals for preventing and minimising the emissions of these substances to be BAT for the Installation subject to the detailed audit referred to below.

(ii) Emissions unlikely to give rise to significant pollution

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Also from the tables above the following emissions (which were not screened out as insignificant) have been assessed as being unlikely to give rise to significant pollution in that the predicted environmental concentration is less than 100% (taking expected modelling uncertainties into account) of both the long term and short term EQS/EAL;

• NO₂, TOC, Cd, Pb, Mn, V, Ni, As and Cr (VI).

For these emissions, we have carefully scrutinised the Applicant's proposals to ensure that they are applying the Best Available Techniques to prevent and minimise emissions of these substances. This is reported in section 6 of this document.

(iii) Emissions requiring further assessment

All emissions either screen out as insignificant or where they do not screen out as insignificant are considered unlikely to give rise to significant pollution.

5.2.2 Consideration of key pollutants

(i) Nitrogen dioxide (NO₂)

The impact on air quality from NO_2 emissions has been assessed against the EU EQS of 40 $\mu g/m^3$ as a long term annual average and a short term hourly average of 200 $\mu g/m^3$. The model assumes a 70% NO_x to NO_2 conversion for the long term and 35% for the short term assessment in line with Environment Agency guidance on the use of air dispersion modelling.

The above tables show that the peak long term PC is greater than 1% of the EUEQS and therefore cannot be screened out as insignificant. Even so, from the table above, the emission is not expected to result in the EUEQS being exceeded. The peak short term PC is below the level we would consider insignificant (>10% of the EUEQS).

(ii) Particulate matter PM₁₀ and PM_{2.5}

The impact on air quality from particulate emissions has been assessed against the EQS for PM_{10} (particles of 10 microns and smaller) and $PM_{2.5}$ (particles of 2.5 microns and smaller). For PM_{10} , the EUEQS are a long term annual average of 40 μ g/m³ and a short term daily average of 50 μ g/m³. For $PM_{2.5}$ the EUEQS of 25 μ g/m³ as a long-term annual average to be achieved by 2010 as a Target Value and by 2015 as a Limit Value has been used.

The Applicant's predicted impact of the Installation against these EQSs is shown in the tables above. The assessment assumes that **all** particulate emissions are present as PM_{10} for the PM_{10} assessment and that **all** particulate emissions are present as $PM_{2.5}$ for the $PM_{2.5}$ assessment.

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The above assessment is considered to represent a worst case assessment in that: -

- It assumes that the plant emits particulates continuously at the IED Annex VI limit for total dust, whereas actual emissions from similar plant are normally lower.
- It assumes all particulates emitted are below either 10 microns (PM₁₀) or 2.5 microns (PM_{2.5}), when some are expected to be larger.

We have reviewed the Applicant's particulate matter impact assessment and are satisfied in the robustness of the Applicant's conclusions.

The above assessment shows that the predicted process contribution for emissions of PM_{10} is below 1% of the long term EQS and below 10% of the short term EQS and so can be considered insignificant. Therefore, generally, we consider the Applicant's proposals for preventing and minimising the emissions of particulates to be BAT for the Installation.

The above assessment also shows that the predicted process contribution for emissions of $PM_{2.5}$ is also below 1% of the Environmental Quality Objective. Therefore the Environment Agency concludes that particulate emissions from the installation, including emissions of PM_{10} or $PM_{2.5}$, will not give rise to significant pollution.

There is currently no emission limit prescribed nor any continuous emissions monitor for particulate matter specifically in the PM_{10} or $PM_{2.5}$ fraction. Whilst the Environment Agency is confident that current monitoring techniques will capture the fine particle fraction ($PM_{2.5}$) for inclusion in the measurement of total particulate matter, an improvement condition has been included that will require a full analysis of particle size distribution in the flue gas, and hence determine the ratio of fine to coarse particles. In the light of current knowledge and available data however the Environment Agency is satisfied that the health of the public would not be put at risk by such emissions, as explained in section 5.3.3.

(iii) Acid gases, SO₂, HCl and HF

From the tables above, emissions of HCl and HF can be screened out as insignificant in that the process contribution is <10% of the short term EQS/EAL. There is no long term EQS/EAL for HCl. HF has 2 assessment criteria – a 1-hr EAL and a monthly EAL – the process contribution is <1% of the monthly EAL and so the emission is insignificant if the monthly EAL is interpreted as representing a long term EAL.

There is no long term EAL for SO₂ for the protection of human health. Protection of ecological receptors from SO₂ for which there is a long term EAL is considered in section 5.4.

Emissions of SO_2 can also be screened out as insignificant in that the short term process contribution is also <10% of each of the three short term EUEQS values. Therefore, generally, we consider the Applicant's proposals

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for preventing and minimising the emissions of these substances to be BAT for the Installation.

(iv) Emissions to Air of CO, TOCs, PAHs, PCBs, Dioxins and NH₃

The above tables show that for CO and VOC emissions, the peak long term PC is less than 1% of the EAL/EQS with the exception of VTOC and the peak short term PC is less than 10% of the EAL/EQS and so can be screened out as insignificant. The tables show that for VTOC emissions, the peak long term PC is greater than 1% of the EAL/EQS and therefore cannot be screened out as insignificant. Even so, from the table above, the emission is not expected to result in the EQS being exceeded.

Therefore, generally, we consider the Applicant's proposals for preventing and minimising the emissions of these substances to be BAT for the Installation.

The Applicant has used the EQS for 1,3 butadiene for their assessment of the impact of VOC. This is based on 1,3 butadiene having the lowest EQS of organic species likely to be present in VOC (other than PAH, PCBs, dioxins and furans). The Applicant has also used the EQS for benzo[a]pyrene (BaP) for their assessment of the impact of PAH. We agree that the use of the BaP EQS is sufficiently precautionary.

There is no EAL for dioxins and furans as the principal exposure route for these substances is by ingestion and the risk to human health is through the accumulation of these substances in the body over an extended period of time. This issue is considered in more detail in section 5.3

From the tables above all the other emissions can be screened out as insignificant in that the process contribution is < 1% of the long term EQS/EAL and <10% of the short term EAQ/EAL, except for TOC where the PC is 3.11% of the long term EAL Even so, from the table above, the emission is not expected to result in the EAL being exceeded.

The ammonia emission is based on a release concentration of 10 mg/m^3 . We are satisfied that this level of emission is consistent with the operation of a well controlled SNCR NO_x abatement system.

Whilst all emissions cannot be screened out as insignificant, the Applicant's modelling shows that the installation is unlikely to result in a breach of the EAL. The Applicant is required to prevent, minimise and control PAH and VOC emissions using the best available techniques, this is considered further in Section 6. We are satisfied that PAH and VOC emissions will not result in significant pollution.

In summary for the above emissions to air, we have carefully scrutinised the Applicant's proposals to ensure that they are applying the Best Available Techniques to prevent and minimise emissions of these substances. This is reported in section 6 of this document. Therefore, generally, we consider the Applicant's proposals for preventing and minimising the emissions of CO,

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NH₃, PAHs and PCBs to be BAT for the Installation. Dioxins and furans are considered further in section 5.3.2.

5.2.3 Assessment of Emission of Metals

The Applicant has assessed the impact of metal emissions to air, as previously described.

Annex VI of IED sets three limits for metal emissions:

- An emission limit value of 0.05 mg/m³ for mercury and its compounds (formerly WID group 1 metal).
- An aggregate emission limit value of 0.05 mg/m³ for cadmium and thallium and their compounds (formerly WID group 2 metals).
- An aggregate emission limit of 0.5 mg/m³ for antimony, arsenic, lead, chromium, cobalt, copper, manganese, nickel and vanadium and their compounds (formerly WID group 3 metals).

In addition the UK is a Party to the Heavy Metals Protocol within the framework of the UN-ECE Convention on long-range trans-boundary air pollution. Compliance with the IED Annex VI emission limits for metals along with the Application of BAT also ensures that these requirements are met.

Where IED sets an aggregate limit, the Applicant's first stage of assessment assumes that each metal is emitted individually at the relevant aggregate emission limit value. This is a something which can never actually occur in practice as it would result in a breach of the limit, and so represents a very much worst case scenario. However using this very conservative assessment approach it can be seen from the tables above that the impact from metals Mercury, Antimony, Chromium and Copper can be considered as insignificant, and the impact from metals Cadmium, Lead, Manganese, Vanadium and Nickel considered unlikely to cause an excedance of an EQS/EAL.

Where IED sets an aggregate limit, the Applicant's second stage of assessment assumes that each metal is emitted as the proportion of metals in its group (i.e. one ninth of the limit for each of the group 3 metals). Historical data for Municipal Waste Incinerators indicates that 1/9th of the limit is an over estimate of actual emissions, and so we are satisfied that the Applicant's proposal is reasonable in this context. Using this precautionary approach to assessment it can be seen from the Revised Impact Assessment table (3) below that it is considered unlikely that the impact from Arsenic will cause an excedance of the EQS/EAL.

Thallium and Cobalt do not have an assigned EAL value. However, as the process contribution of these metals is similar to that of the other metals, we consider the emissions of these metals to be not significant.

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In summary, from the data presented in the tables at section 5.2.1 above and the impact assessment criteria described subsequently, we are satisfied that the emissions of the following metals can be screened out as being insignificant:

Mercury, Antimony, Chromium and Copper

and that the following metal emissions whilst not able to be screened out as insignificant, are assessed as being unlikely to give rise to an impact that will give rise to excedance of an EAL/EQS:

Cadmium, Lead, Manganese, Vanadium, Nickel and Arsenic.

There are no metal emissions requiring further assessment. From their assessment, the Applicant has concluded that exceedences of the EAL for all metals is not likely to occur. The Installation has been assessed as meeting BAT for control of metal emissions to air. See section 6 of this document. The Environment Agency's experience of regulating incineration plant is that emissions of metals are in any event below the limits set in IED. We therefore agree with the Applicant's conclusions.

The 2009 report of the Expert Panel on Air Quality Standards (EPAQS) – "Guidelines for Metal and Metalloids in Ambient Air for the Protection of Human Health", sets new ambient air quality guidelines for Arsenic, Nickel and Chromium (VI). These guidelines have been incorporated as EALs in the revised H1 Guidance issued by the Agency in 2010.

Chromium (VI) is not specifically referenced in WID, which includes only total Chromium as one of the nine Group 3 metals, the impact of which has been assessed above. The EPAQS guidelines refer only to that portion of the metal emissions contained within PM_{10} in ambient air. The new guideline for Chromium (VI) is 0.2 ng/m^3 .

• Measurement of Chromium (VI) at the levels anticipated at the stack emission points is expected to be difficult, with the likely levels being below the level of detection by the most advanced methods. We have considered the concentration of total chromium and chromium (VI) in the APC residues collected upstream of the emission point for existing Municipal Waste incinerators and have assumed these to be similar to the particulate matter released from the emission point. This data shows that the mean Cr (VI) emission concentration (based on the bag dust ratio) is 3.5 * 10⁻⁵ mg/m³ (max 1.3 * 10⁻⁴).

Based on this data, we consider it remains a conservative assumption for the Applicant to consider in their final stage assessment that the Cr(VI) emission concentration will be 8.2 * 10^{-5} mg/m³.

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In their impact assessment of Cr(VI) emissions the Applicant has made reference to the Agency guidance document "Guidance to Applicants on Impact Assessment for Group 3 Metals Stack Releases – V.2 June 2011". Although this guidance document was updated in September 2012 (Guidance to Applicants on Impact Assessment for Group 3 Metals Stack Releases – V.3 September 2012"), we are satisfied that the basis they have used to quantify likely Cr(VI) emission remains valid and in accordance with the updated quidance.

In their assessment the Applicant has presented Cr(VI) background data based on information obtained from the UK Emissions of Air Pollutants 1970 to 2008 records. However there is little data available on the background levels of Cr(VI); so we have assumed this to be 20% of the total Cr background level, 20% is the typical value of Cr(VI) in total Cr reported in the environment in the EPAQS Guidelines. The background data for Cr(VI) presented in the table above therefore reflects this assumption.

The Applicant has used the above data to model the predicted Cr(VI) impact. The PC is predicted as 0.44%, which we consider to be negligible as an additional impact.

This assessment shows that emissions of Chromium (VI) are likely to be insignificant, and we agree with the Applicant's conclusions.

The table below summarises the revised impact assessment based on the assumptions detailed above.

Revised Assessment of Emissions to Air (3)

Pollutant	EQS/ EAL		Back- ground	Process Contribut	ion	Predicted Environme Concentra	ental
	μg/m³		μg/m³	μg/m³	% of EAL	μg/m³	% of EAL
As	0.003	1	0.00148	0.00038	12.66	0.00186	61.9
Cr (VI)	0.0002	1	0.00050	0.0034	0.44	-	-

The predicted PC for Arsenic is above 1% of the EQS/EAL however taking the background concentration into account the PEC is 61.9% and there is sufficient headroom that it is considered unlikely that the impact from Arsenic will cause an excedance of the EQS/EAL.

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The predicted PC for Chromium (VI) is 0.44% of the EAL/EQS and as it is below 1% screens out from further assessment. This assessment shows that emissions of Chromium (VI) are likely to be insignificant.

In addition improvement condition IC5 has been included in the permit for the Operator to re-assess the impacts based on the assumptions made for arsenic and Chromium and to provide further actions should there be significant deviation from these assumptions that suggests an exceedance of the EAL/EQS.

5.2.4 Consideration of Local Factors

The installation is located in close proximity to the Mersey Estuary SPA/Ramsar and therefore additional measures to control NOx emissions have been proposed by the operator as detailed in section 5.2.5 below.

Wirral Borough Council has not declared an Air Quality Management Area (AQMA) within the borough however neighbouring boroughs Cheshire West and Chester and Liverpool have both declared AQMAs due to elevated nitrogen dioxide concentrations due to road traffic emissions. The closest AQMAs are:

- Whitby Road / Station Road, Ellesmere Port AQMA approximately 5 km to the south-east of the facility; and
- Liverpool City AQMA approximately 4 km to the east of the facility on the opposite bank of the River Mersey.

From the Applicants model, the process contribution at all points within each of the AQMAs is predicted to be well below 1% of the EUEQS and can therefore be considered insignificant.

The Applicant is required to prevent, minimise and control emissions using the best available techniques; this is considered further in Section 6.

5.2.5 Consideration of Additional Measures to Control Emissions

The operator has proposed and we have set a NOx limit less than Annex IV of IED for emission point A1 as detailed below because this can be achieved by using Selective Catalytic Reduction (SCR) abatement and the installation is located in close proximity to the Mersey Estuary SPA/Ramsar.

Emission point A1

- NOx reduced emission limit value for 24 hour daily of 100 mg/m³ compared with 200 mg/m³ as detailed in Annex IV of IED.
- NOx 220 mg/m³ reduced emission limit value for ½ hour limit compared with the Annex IV of IED limit of 400 mg/m³.

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5.3 Human health risk assessment

5.3.1 Our role in preventing harm to human health

The Environment Agency has a statutory role to protect the environment and human health from all processes and activities it regulates. We assessed the effects on human health for this application in the following ways:

i) Applying Statutory Controls

The plant will be regulated under EPR. These regulations include the requirements of relevant EU Directives, notably, the industrial emissions directive (IED), the waste framework directive (WFD), and ambient air directive (AAD).

The main conditions in an EfW permit are based on the requirements of the IED. Specific conditions have been introduced to specifically ensure compliance with the requirements of Chapter IV. The aim of the IED is to prevent or, where that is not practicable, to reduce emissions to air, water and land and prevent the generation of waste, in order to achieve a high level of protection of the environment taken as a whole. IED achieves this aim by setting operational conditions, technical requirements and emission limit values to meet the requirements set out in Articles 11 and 18 of the IED. These requirements include the application of BAT, which may in some circumstances dictate tighter emission limits and controls than those set out in Chapter IV of IED on waste incineration and co-incineration plants. The assessment of BAT for this installation is detailed in section 6 of this document.

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ii) Environmental Impact Assessment

Industrial activities can give rise to odour, noise and vibration, accidents, fugitive emissions to air and water, releases to air (including the impact on Photochemical Ozone Creation Potential (POCP)), discharges to ground or groundwater, global warming potential and generation of waste. For an installation of this kind, the principal environmental effects are through emissions to air, although we also consider all of the other impacts listed. Section 5.1 and 5.2 above explain how we have approached the critical issue of assessing the likely impact of the emissions to air from the Installation on human health and the environment and any measures we are requiring to ensure a high level of protection.

iii) Expert Scientific Opinion

We take account of the views of national and international expert bodies. Following is a summary of some of the publications which we have considered (in no particular order).

An independent review of evidence on the health effects of municipal waste incinerators was published by **DEFRA** in 2004. It concluded that there was no convincing link between the emissions from MSW incinerators and adverse effects on public health in terms of cancer, respiratory disease or birth defects. On air quality effects, the report concluded "Waste incinerators contribute to local air pollution. This contribution, however, is usually a small proportion of existing background levels which is not detectable through environmental monitoring (for example, by comparing upwind and downwind levels of airborne pollutants or substances deposited to land). In some cases, waste incinerator facilities may make a more detectable contribution to air pollution. Because current MSW incinerators are located predominantly in urban areas, effects on air quality are likely to be so small as to be undetectable in practice."

HPA (now PHE) in 2009 states that "The Health Protection Agency has reviewed research undertaken to examine the suggested links between emissions from municipal waste incinerators and effects on health. While it is not possible to rule out adverse health effects from modern, well regulated municipal waste incinerators with complete certainty, any potential damage to the health of those living close-by is likely to be very small, if detectable".

Policy Advice from Government also points out that the minimal risk from modern incinerators. Paragraph 22 (Chapter 5) of WS2007 says that "research carried out to date has revealed no credible evidence of adverse health outcomes for those living near incinerators." It points out that "the relevant health effects, mainly cancers, have long incubation times. But the research that is available shows an absence of symptoms relating to exposures twenty or more years ago when emissions from incinerators were much greater than is now the case." Paragraph 30 of PPS10 explains that "modern, appropriately located, well run and well regulated waste management facilities should pose little risk to public health."

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The Committee on Carcinogenicity of Chemicals in Food, Consumer Products and the Environment (CoC) issued a statement in 2000 which said that "any potential risk of cancer due to residency (for periods in excess of 10 years) near to municipal solid waste incinerators was exceedingly low and probably not measurable by the most modern epidemiological techniques." In 2009, CoC considered six further relevant epidemiological papers that had been published since the 2000 statement, and concluded that "there is no need to change the advice given in the previous statement in 2000 but that the situation should be kept under review".

Republic of Ireland Health Research Board report stated that "It is hard to separate the influences of other sources of pollutants, and other causes of cancer and, as a result, the evidence for a link between cancer and proximity to an incinerator is not conclusive".

The Food Safety Authority of Ireland (FSAI) (2003) investigated possible implications on health associated with food contamination from waste incineration and concluded: "In relation to the possible impact of introduction of waste incineration in Ireland, as part of a national waste management strategy, on this currently largely satisfactory situation, the FSAI considers that such incineration facilities, if properly managed, will not contribute to dioxin levels in the food supply to any significant extent. The risks to health and sustainable development presented by the continued dependency on landfill as a method of waste disposal far outweigh any possible effects on food safety and quality."

Health Protection Scotland (2009) considered scientific studies on health effects associated with the incineration of waste particularly those published after the Defra review discussed earlier. The main conclusions of this report were: "(a) For waste incineration as a whole topic, the body of evidence for an association with (non-occupational) adverse health effects is both inconsistent and inconclusive. However, more recent work suggests, more strongly, that there may have been an association between emissions (particularly dioxins) in the past from industrial, clinical and municipal waste incinerators and some forms of cancer, before more stringent regulatory requirements were implemented. (b) For individual waste streams, the evidence for an association with (non-occupational) adverse health effects is inconclusive. (c) The magnitude of any past health effects on residential populations living near incinerators that did occur is likely to have been small. (d) Levels of airborne emissions from individual incinerators should be lower now than in the past. due to stricter legislative controls and improved technology. Hence, any risk to the health of a local population living near an incinerator, associated with its emissions, should also now be lower."

The US National Research Council Committee on Health Effects of Waste Incineration (NRC) (NRC 2000) reviewed evidence as part of a wide ranging report. The Committee view of the published evidence was summarised in a key conclusion: "Few epidemiological studies have attempted to assess whether adverse health effects have actually occurred

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near individual incinerators, and most of them have been unable to detect any effects. The studies of which the committee is aware that did report finding health effects had shortcomings and failed to provide convincing evidence. That result is not surprising given the small populations typically available for study and the fact that such effects, if any, might occur only infrequently or take many years to appear. Also, factors such as emissions from other pollution sources and variations in human activity patterns often decrease the likelihood of determining a relationship between small contributions of pollutants from incinerators and observed health effects. Lack of evidence of such relationships might mean that adverse health effects did not occur, but it could mean that such relationships might not be detectable using available methods and sources."

The British Society for Ecological Medicine (BSEM) published a report in 2005 on the health effects associated with incineration and concluded that "Large studies have shown higher rates of adult and childhood cancer and also birth defects around municipal waste incinerators: the results are consistent with the associations being causal. A number of smaller epidemiological studies support this interpretation and suggest that the range of illnesses produced by incinerators may be much wider. Incinerator emissions are a major source of fine particulates, of toxic metals and of more than 200 organic chemicals, including known carcinogens, mutagens, and hormone disrupters. Emissions also contain other unidentified compounds whose potential for harm is as yet unknown, as was once the case with dioxins. Abatement equipment in modern incinerators merely transfers the toxic load, notably that of dioxins and heavy metals, from airborne emissions to the fly ash. This fly ash is light, readily windborne and mostly of low particle size. It represents a considerable and poorly understood health hazard."

The BSEM report was reviewed by the HPA and they concluded that "Having considered the BSEM report the HPA maintains its position that contemporary and effectively managed and regulated waste incineration processes contribute little to the concentrations of monitored pollutants in ambient air and that the emissions from such plants have little effect on health." The BSEM report was also commented on by the consultants who produced the Defra 2004 report referred to above. They said that "It fails to consider the significance of incineration as a source of the substances of concern. It does not consider the possible significance of the dose of pollutants that could result from incinerators. It does not fairly consider the adverse effects that could be associated with alternatives to incineration. It relies on inaccurate and outdated material. In view of these shortcomings, the report's conclusions with regard to the health effects of incineration are not reliable."

A **Greenpeace** review on incineration and human health concluded that a broad range of health effects have been associated with living near to incinerators as well as with working at these installations. Such effects include cancer (among both children and adults), adverse impacts on the respiratory system, heart disease, immune system effects, increased allergies and congenital abnormalities. Some studies, particularly those on cancer, relate to

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old rather than modern incinerators. However, modern incinerators operating in the last few years have also been associated with adverse health effects."

The Health Protection Scotland report referred to above says that "the authors of the Greenpeace review do not explain the basis for their conclusion that there is an association between incineration and adverse effects in terms of criteria used to assess the strength of evidence. The weighting factors used to derive the assessment are not detailed. The objectivity of the conclusion cannot therefore be easily tested."

From this published body of scientific opinion, we take the view stated by the HPA that "While it is not possible to rule out adverse health effects from modern, well regulated municipal waste incinerators with complete certainty, any potential damage to the health of those living close-by is likely to be very small, if detectable". We therefore ensure that permits contain conditions which require the installation to be well-run and regulate the installation to ensure compliance with such permit conditions.

iv) Health Risk Models

Comparing the results of air dispersion modelling as part of the H1 Environmental Impact assessment against European and national air quality standards effectively makes a health risk assessment for those pollutants for which a standard has been derived. These air quality standards have been developed primarily in order to protect human health via known intake mechanisms, such as inhalation and ingestion. Some pollutants, such as dioxins, furans and dioxin like PCB's, have human health impacts at lower ingestion levels than lend themselves to setting an air quality standard to control against. For these pollutants, a different human health risk model is required which better reflects the level of dioxin intake.

Models are available to predict the dioxin, furan and dioxin like PCB's intake for comparison with the Tolerable Daily Intake (TDI) recommended by the Committee on Toxicity of Chemicals in Food, Consumer Products and the Environment, known as COT. These include HHRAP and the HMIP model.

HHRAP has been developed by the US EPA to calculate the human body intake of a range of carcinogenic pollutants and to determine the mathematic quantitative risk in probabilistic terms. In the UK, in common with other European Countries, we consider a threshold dose below which the likelihood of an adverse effect is regarded as being very low or effectively zero. The HMIP model uses a similar approach to the HHRAP model, but does not attempt to predict probabilistic risk. Either model can however be used to make comparisons with the TDI.

The TDI is the amount of a substance that can be ingested daily over a lifetime without appreciable health risk. It is expressed in relation to bodyweight in order to allow for different body size, such as for children of different ages. In the UK, the COT has set a TDI for dioxins, furans and

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dioxin like PCB's of 2 picograms I-TEQ/Kg-body weight/day (N.B. a picogram is a million millionths (10⁻¹²) of a gram).

In addition to an assessment of risk from dioxins, furans and dioxin like PCBs the HHRAP model enables a risk assessment from human intake of a range of heavy metals. The HMIP report does not consider metals and PCB's. In principle, the respective EQS for these metals are protective of human health. It is not therefore necessary to model the human body intake.

COMEAP developed a methodology based on the results of time series epidemiological studies which allows calculation of the public health impact of exposure to the classical air pollutants (NO₂, SO₂ and particulates) in terms of the numbers of "deaths brought forward" and the "number of hospital admissions for respiratory disease brought forward or additional". COMEAP has issued a statement expressing some reservations about the applicability of applying its methodology to small affected areas. Those concerns generally relate to the fact that the exposure-response coefficients used in the COMEAP report derive from studies of whole urban populations where the air pollution climate may differ from that around a new industrial installation. COMEAP identified a number of factors and assumptions that would contribute to the uncertainty of the estimates. These were summarised in the Defra review as below:

- Assumption that the spatial distribution of the air pollutants considered is the same in the area under study as in those areas, usually cities or large towns, in which the studies which generated the coefficients were undertaken.
- Assumption that the temporal pattern of pollutant concentrations in the area under study is similar to that in the areas in which the studies which generated the coefficients were undertaken (i.e. urban areas).
- It should be recognised that a difference in the pattern of socioeconomic conditions between the areas to be studied and the reference areas could lead to inaccuracy in the predicted level of effects.
- In the same way, a difference in the pattern of personal exposures between the areas to be studied and the reference areas will affect the accuracy of the predictions of effects.

The use of the COMEAP methodology is not generally recommended for modelling the human health impacts of individual installations. However it may have limited applicability where emissions of NO_x , SO_2 and particulates cannot be screened out as insignificant in an H1 Environmental Impact assessment, there are high ambient background levels of these pollutants and we are advised that its use was appropriate by our public health consultees.

Our recommended approach is therefore the use of the H1 assessment methodology comparison for most pollutants (including metals) and dioxin intake model using the HHRAP model as described above for dioxins, furans and dioxin like PCBs. Where an alternative approach is adopted for dioxins, we check the predictions ourselves.

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v) Consultations

As part of our normal procedures for the determination of a permit application, we would consult Directors of Public Health, FSA and PHE. We also consult the local communities who may raise health related issues. All issues raised by these consultations are considered in determining the application as described in Annex 4 of this document.

5.3.2 Assessment of Intake of Dioxins, Furans and Dioxin like PCBs

For dioxins, furans and dioxin like PCBs, the principal exposure route is through ingestion, usually through the food chain, and the main risk to health is through accumulation in the body over a period of time.

The human health risk assessment calculates the dose of dioxins and furans that would be received by local receptors if all their food and water were sourced from the locality where the deposition of dioxins and furans is predicted to be the highest. This is then assessed against the Tolerable Daily Intake (TDI) levels established by the COT of 2 picograms I-TEQ / Kg bodyweight/ day.

The results of the Applicant's assessment of dioxin intake are detailed in the table below. (worst – case results for each category are shown). The results showed that the predicted daily intake of dioxins at all receptors, resulting from emissions from the proposed facility, were significantly below the recommended TDI levels. We therefore consider the intake of dioxins and furans resulting from operation of the proposed Installation to be insignificant, and believe it is unlikely that the COT TDI level of 2 picograms I-TEQ / Kg bodyweight/ day will be exceeded.

Receptor	Adult	Child
Resident	0.000606	0.00158
Farmer	0.0104	0.01207

Calculated maximum daily intake of dioxins by local receptors resulting from the operation of the proposed facility (picograms I-TEQ/ kg-BW/day)

The FSA has reported that dietary studies have shown that estimated total dietary intakes of dioxins and dioxin-like PCBs from all sources by all age groups fell by around 50% between 1997 and 2001, and are expected to continue to fall. In 2001, the average daily intake by adults in the UK from diet was 0.9 pg WHO-TEQ/kg bodyweight. The additional daily intake predicted by the modelling as shown in the table above is substantially below this figure.

In 2010, FSA studied the levels of chlorinated, brominated and mixed (chlorinated-brominated) dioxins and dioxin-like PCBs in fish, shellfish, meat and eggs consumed in UK. It asked COT to consider the results and to advise on whether the measured levels of these PXDDs, PXDFs and PXBs indicated a health concern ('X' means a halogen). COT issued a statement in December 2010 and concluded that "The major contribution to the total dioxin toxic activity in the foods measured came from chlorinated compounds.

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Brominated compounds made a much smaller contribution, and mixed halogenated compounds contributed even less (1% or less of TDI). Measured levels of PXDDs, PXDFs and dioxin-like PXBs do not indicate a health concern". COT recognised the lack of quantified TEFs for these compounds but said that "even if the TEFs for PXDDs, PXDFs and dioxin-like PXBs were up to four fold higher than assumed, their contribution to the total TEQ in the diet would still be small. Thus, further research on PXDDs, PXDFs and dioxin-like PXBs is not considered a priority."

In the light of this statement, we assess the impact of chlorinated compounds as representing the impact of all chlorinated, brominated and mixed dioxins / furans and dioxin like PCBs.

5.3.3 Particulates smaller than 2.5 microns

The Operator will be required to monitor particulate emissions using the method set out in Table S3.1 of Schedule 3 of the Permit. This method requires that the filter efficiency must be at least 99.5 % on a test aerosol with a mean particle diameter of 0.3 μm , at the maximum flow rate anticipated. The filter efficiency for larger particles will be at least as high as this. This means that particulate monitoring data effectively captures everything above 0.3 μm and much of what is smaller. It is not expected that particles smaller than 0.3 μm will contribute significantly to the mass release rate / concentration of particulates because of their very small mass, even if present. This means that emissions monitoring data can be relied upon to measure the true mass emission rate of particulates.

Nano-particles are considered to refer to those particulates less than 0.1 μ m in diameter (PM_{0.1}). Questions are often raised about the effect of nanoparticles on human health, in particular on children's health, because of their high surface to volume ratio, making them more reactive, and their very small size, giving them the potential to penetrate cell walls of living organisms. The small size also means there will be a larger number of small particles for a given mass concentration. However the HPA statement (referenced below) says that due to the small effects of incinerators on local concentration of particles, it is highly unlikely that there will be detectable effects of any particular incinerator on local infant mortality.

The HPA addresses the issue of the health effects of particulates in their September 2009 statement 'The Impact on Health of Emissions to Air from Municipal Incinerators'. It refers to the coefficients linking PM_{10} and $PM_{2.5}$ with effects on health derived by COMEAP and goes on to say that if these coefficients are applied to small increases in concentrations produced, locally, by incinerators; the estimated effects on health are likely to be small. The HPA notes that the coefficients that allow the use of number concentrations in impact calculations have not yet been defined because the national experts have not judged that the evidence is sufficient to do so. This is an area being kept under review by COMEAP.

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In December 2010, COMEAP published a report on The Mortality Effects of Long-Term Exposure to Particulate Air Pollution in the United Kingdom. It says that "a policy which aims to reduce the annual average concentration of $PM_{2.5}$ by 1 μ g/m³ would result in an increase in life expectancy of 20 days for people born in 2008." However, "The Committee stresses the need for careful interpretation of these metrics to avoid incorrect inferences being drawn — they are valid representations of population aggregate or average effects, but they can be misleading when interpreted as reflecting the experience of individuals."

The HPA (now PHE) also point out that in 2007 incinerators contributed 0.02% to ambient ground level PM_{10} levels compared with 18% for road traffic and 22% for industry in general. The HPA note that in a sample collected in a day at a typical urban area the proportion of $PM_{0.1}$ is around 5-10% of PM_{10} . It goes on to say that PM_{10} includes and exceeds $PM_{2.5}$ which in turn includes and exceeds $PM_{0.1}$.

This is consistent with the assessment of this application which shows emissions of PM_{10} to air to be insignificant.

We take the view, based on the foregoing evidence, that techniques which control the release of particulates to levels which will not cause harm to human health will also control the release of fine particulate matter to a level which will not cause harm to human health.

5.3.4 Assessment of Health Effects from the Installation

We have assessed the health effects from the operation of this installation in relation to the above (sections 5.3.1 to 5.3.3). We have applied the relevant requirements of the national and European legislation in imposing the permit conditions. We are satisfied that compliance with these conditions will ensure protection of the environment and human health.

Taking into account all of the expert opinion available, we agree with the conclusion reached by the HPA that "While it is not possible to rule out adverse health effects from modern, well regulated municipal waste incinerators with complete certainty, any potential damage to the health of those living close-by is likely to be very small, if detectable."

In carrying out air dispersion modelling as part of the H1 Environmental Impact assessment and comparing the predicted environmental concentrations with European and national air quality standards, the Applicant has effectively made a health risk assessment for many pollutants. These air quality standards have been developed primarily in order to protect human health.

The Applicant's assessment of the impact from PM_{10} , $PM_{2.5}$, SO_2 , HCI, HF, CO, PAH, NH_3 , PCBs, Dioxins, Hg, Sb, Co, Cu and Cr (II) (III) have all indicated that the Installation emissions screen out as insignificant; where the impact of emissions of NO_2 , TOC, Cd, Pb, Mn, V, Ni, As and Cr (VI) have not

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been screened out as insignificant, the assessment still shows that the predicted environmental concentrations are well within air quality standards or environmental action levels.

The Environment Agency has reviewed the methodology employed by the Applicant to carry out the health impact assessment. Generally, the Applicant's assessment methodology is acceptable. We did raise some queries regarding the Applicant's assessment, but the issues were minor, mainly for clarification and did not affect the impact assessment conclusions. Based on the emission limit values and the Applicant's assumptions, our check modelling indicates that the Applicant's conclusions are acceptable at the selected receptors.

Overall, taking into account the conservative nature of the impact assessment (i.e. that it is based upon an individual exposed for a life-time to the effects of the highest predicted airborne concentrations and consuming mostly locally grown food), it was concluded that the operation of the proposed facility will not pose a significant carcinogenic or non-carcinogenic risk to human health. Public Health England, Wirral Metropolitan Borough Council – Planning Department and Wirral Metropolitan Borough Council – Environmental Protection Department were consulted on the Application and concluded that they had no significant concerns regarding the risk to the health of humans from the installation. The Food Standards Agency was also consulted during the permit determination process and it concluded that it is unlikely that there will be any unacceptable effects on the human food chain as a result of the operations at the Installation. Details of the responses provided by the PCT / Local Health Board, PHE and FSA to the consultation on this Application can be found in Annex 2.

The Environment Agency is therefore satisfied that the Applicant's conclusions presented above are soundly based and we conclude that the potential emissions of pollutants including dioxins, furans and metals from the proposed facility are unlikely to have an impact upon human health.

5.4 Impact on Habitats sites, SSSIs, non-statutory conservation sites etc.

5.4.1 <u>Sites Considered</u>

The following Habitats (i.e. Special Areas of Conservation, Special Protection Areas and Ramsar) sites are located within 10km of the Installation:

- Mersey Estuary SPA, Ramsar
- Dee Estuary SPA, SAC, Ramsar

The following Sites of Special Scientific Interest are located within 2km of the Installation:

Mersey Estuary

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The following non-statutory local wildlife and conservation sites are located within 2km of the Installation:

- Sale Wood (Ancient Woodland)
- Rivacre Valley (LWS)
- Booston Wood (LWS)

5.4.2 <u>Habitats Assessment</u>

The Applicant's Habitats assessment was reviewed by the Environment Agency's technical specialists for modelling, air quality, conservation and ecology technical services, who agreed with the assessment's conclusions, that there would be no likely significant effect on the interest feature(s) of the protected site(s).

Pollutant	EQS / EAL (µg/m³)	Back- ground (µg/m³)	Process Contribution (PC) (µg/m³)	PC as % of EQS / EAL	Predicted Environmental Concentration (PEC) (µg/m³)	PEC as % EQS / EAL
Direct Impact	S					
NO _x Annual	30	32.74	0.68	2.3	33.42	111.4
NO _x Daily Mean	75	32.74	11.61	35.5	44.35	59.1
SO ₂	20	6.80	0.34	1.7	7.14	35.7
Ammonia	3	1.31	0.07	2.3	1.38	46.0
HF Weekly Mean	0.5	-	0.03	6.0	-	-
HF Daily Mean	5	-	0.12	2.4	-	-
Deposition In	npacts					
N Deposition (kg N/ha/yr)	20 - 30	20.16	0.422	2.11	20.582	102.91
Acidification - Nitrogen Dep (Keq/ha/yr)	N/A ⁽¹⁾	-	-	-	-	-
Acidification Sulphur Dep (Keq/ha/yr)	N/A ⁽¹⁾	-	-	-	-	-

(1) Mersey Estuary not sensitive to acid deposition – no assessment required.

From the table above all of the emissions apart from short and long term emissions of nitrogen dioxide and nitrogen nutrient deposition on the Mersey Estuary SPA/Ramsar can be screened out as insignificant and their impact considered not discernable, in that the process contribution is < 1% of the

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long term EQS/EAL and <10% of the short term EAQ/EAL (Critical Level or Critical Load).

More comprehensive details of our assessment of impact on the Habitat sites is recorded in our Appendix 11 assessment document – our initial assessment concluded that there was the potential for a significant effect on the Mersey Estuary SPA/Ramsar due to emissions of nitrogen dioxide and nitrogen nutrient deposition. This assessment was sent to Natural England for their consultation review and approval. Their response concluded that the emissions from the installation were unlikely to have a significant effect on any European site, and could therefore be screened out from any requirement for further assessment under the Habitats Regulations, the relevant European sites had no habitat features sensitive to air pollution impacts (e.g., geological or freshwater sites with no vegetative features sensitive to air pollution) or the modelling showed that areas of sensitive habitat within the sites would not be affected by the proposed development.

Taking into account the response from Natural England and the minor contribution of emissions from the process to existing background levels we conclude that emissions from the proposed Installation will not have any likely significant effect on the features of the Habitat sites.

We are therefore satisfied that the Applicants assessment of impact on the relevant Habitat sites is satisfactory and consider that the operation of the proposed Installation will not have an adverse effect on the features of these Habitat sites.

5.4.3 SSSI Assessment

The Applicant's assessment of SSSIs was reviewed by the Environment Agency's technical specialists for modelling, air quality, conservation and ecology technical services, who agreed with the assessment's conclusions, that the proposal does not damage the special features of the SSSI(s).

The Mersey Estuary SSSI location is consistent with the Mersey Estuary SPA/Ramsar and the detailed modelling and associated conclusions for the habitats assessment above are valid.

We are therefore satisfied that the Applicants assessment of impact on the relevant SSSI is satisfactory and consider that the operation of the proposed Installation will not cause damage to the SSSI.

5.4.4 Assessment of Non-Statutory Sites

We have a duty under the Environment Act 1995 to ensure that there will be no significant impact on non-statutory sites. The Environment Agency considers that the emission of a pollutant will not be significant if the process contribution (PC), predicted by atmospheric dispersion modelling, is less than 100% of the relevant critical level or load.

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All process contributions at the maximum ground level concentration (see section 5.4.2 above) are significantly below the relevant critical level or load and these impacts are higher than would be experienced at the nearest Non-Statutory Site (Rivacre Wood LWS). The site is 0.8km away, further than the impacts assessment and therefore the process contribution would be less due to further atmospheric dispersion and we can conclude that there will be no significant pollution at any of the Non-Statutory Sites.

5.5 <u>Impact of abnormal operations</u>

Article 50(4)(c) of IED requires that waste incineration and co-incineration plants shall operate an automatic system to prevent waste feed whenever any of the continuous emission monitors show that an emission limit value (ELV) is exceeded due to disturbances or failures of the purification devices. Notwithstanding this, Article 46(6) allows for the continued incineration and co-incineration of waste under such conditions provided that this period does not (in any circumstances) exceed 4 hours uninterrupted continuous operation or the cumulative period of operation does not exceed 60 hours in a calendar year. This is a recognition that the emissions during transient states (e.g. start-up and shut-down) are higher than during steady-state operation, and the overall environmental impact of continued operation with a limited exceedance of an ELV may be less than that of a partial shut-down and restart.

For incineration plant, IED sets backstop limits for particulates, CO and TOC which must continue to be met at all times. The CO and TOC limits are the same as for normal operation, and are intended to ensure that good combustion conditions are maintained. The backstop limit for particulates is 150 mg/m³ (as a half hourly average) which is five times the limit in normal operation.

Article 45(1)(f) requires that the permit shall specify the maximum permissible period of any technically unavoidable stoppages, disturbances, or failures of the purification devices or the measurement devices, during which the concentrations in the discharges into the air may exceed the prescribed emission limit values. In this case we have decided to set the time limit at 4 hours, which is the maximum period prescribed by Article 46(6).

Given that these abnormal operations are limited to no more than a period of 4 hours continuous operation and no more than 60 hour aggregated operation in any calendar year. This is less than 1% of total operating hours and so abnormal operating conditions are not expected to have any significant long term environmental impact unless the background conditions were already close to, or exceeding, an EQS. For the most part therefore consideration of abnormal operations is limited to consideration of its impact on short term EQSs.

In making an assessment of abnormal operations the following worst case scenario has been assumed:

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- Dioxin emissions of 10 ng/m³ (100 x normal)
- Mercury emissions are 15 times those of normal operation
- NO_x emissions of 550 mg/m³ (1.38 x normal)
- Particulate emissions of 150 mg/m³ (5 x normal)
- Metal emissions are 15 times those of normal operation
- SO₂ emissions of 480 mg/m³ (2.4 x normal)
- HCl emissions of 900 mg/m³ (15 x normal)

This is a worst case scenario in that these abnormal conditions include a number of different equipment failures not all of which will necessarily result in an adverse impact on the environment (e.g. a failure of a monitoring instrument does not necessarily mean that the incinerator or abatement plant is malfunctioning). This analysis assumes that any failure of any equipment results in all the negative impacts set out above occurring simultaneously.

The result on the Applicant's short-term environmental impact is summarised in the table below.

Assessment of Emissions to Air (3)

Pollutant	t EQS / EAL		Back- ground	Process Contribution (PC)		Predicted Environmental Concentration (PEC)	
	μg/m [°]	3	μg/m³	μg/m³	% of EAL	μg/m³	% of EAL
NO ₂	200	2	59.48	23.29	11.6	82.77	41.4
PM ₁₀	50	3	33.46	3.5	7.00	36.96	73.9
SO ₂	266	4	22.6	64.13	24.1	86.73	32.6
	350	5	22.6	86.92	24.83	109.52	31.3
HCI	750	6	1.06	241.44	32.192	242.5	32.33
HF	160	6	4.7	24.14	15.0875	28.84	18.0
Hg	7.5	1	0.0466	0.2012	2.68	0.24780	3.304
Sb	150	1	0	0.04628	0.03	0.04628	0.031
Cu	200	1	0.01484	0.06559	0.03	0.08043	0.040
Mn	1500	1	0.01958	0.14688	0.01	0.16646	0.0111
Cr (II)(III)	150	1	0.00496	0.20965	0.14	0.21461	0.1431
Dioxins			3.9E-08	6.8E-08		1.46E-07	

- 1 1-hr Maximum
- 2 99.79th %ile of 1-hour mean
- 3 90.41st %ile of 24-hour mean
- 4 99.9th %ile of 15-min mean
- 5 99.73rd %ile of 1-hour mean
- 6 1-hour average

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From the table above the emissions of the following substances can still be considered insignificant, in that the PC is still <10% of the short-term EQS/EAL: PM₁₀, Hg, Sb, Cu, Mn and Cr (II)(III).

Also from the table above emissions of the following emissions (which were not screened out as insignificant) have been assessed as being unlikely to give rise to significant pollution in that the predicted environmental concentration is less than 100% of short term EQS/EAL; NO₂, SO₂, HCl and HF.

We are therefore satisfied that it is not necessary to further constrain the conditions and duration of the periods of abnormal operation beyond those permitted under Chapter IV of the IED.

We have not assessed the impact of abnormal operations against long term EQSs for the reasons set out above. Except that if dioxin emissions were at 10 ng/m³ for the maximum period of abnormal operation, this would result in an increase of approximately 68% in the TDI reported in section 5.3.2. In these circumstances the TDI would be 0.0203 pg(I-TEQ/ kg-BW/day) for the worst case scenario of the farmer's child, which is 1.007% of the COT TDI. At this level, emissions of dioxins will still not pose a risk to human health.

6. Application of Best Available Techniques

6.1 Scope of Consideration

In this section, we explain how we have determined whether the Applicant's proposals are the Best Available Techniques for this Installation.

- The first issue we address is the fundamental choice of incineration technology. There are a number of alternatives, and the Applicant has explained why it has chosen one particular kind for this Installation.
 - We then consider in particular control measures for the emissions which were not screened out as insignificant in the previous section on minimising the installation's environmental impact. They are: NO₂, TOC, Cd, Pb, Mn, V, Ni, As and Cr (VI).
- We also have to consider the combustion efficiency and energy utilisation
 of different design options for the Installation, which are relevant
 considerations in the determination of BAT for the Installation, including
 the Global Warming Potential of the different options.
- Finally, the prevention and minimisation of Persistent Organic Pollutants (POPs) must be considered, as we explain below.

Chapter IV of the IED specifies a set of maximum emission limit values. Although these limits are designed to be stringent, and to provide a high level

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of environmental protection, they do not necessarily reflect what can be achieved by new plant. Article 14(3) of the IED says that BAT conclusions shall be the reference for setting the permit conditions, so it may be possible and desirable to achieve emissions below the limits referenced in Chapter IV.

Even if the Chapter IV limits are appropriate, operational controls complement the emission limits and should generally result in emissions below the maximum allowed; whilst the limits themselves provide headroom to allow for unavoidable process fluctuations. Actual emissions are therefore almost certain to be below emission limits in practice, because any Operator who sought to operate its installation continually at the maximum permitted level would almost inevitably breach those limits regularly, simply by virtue of normal fluctuations in plant performance, resulting in enforcement action (including potentially prosecution) being taken. Assessments based on, say, Chapter IV limits are therefore "worst-case" scenarios.

Should the Installation, once in operation, emit at rates significantly below the limits included in the Permit, we will consider tightening ELVs appropriately. We are, however, satisfied that emissions at the permitted limits would ensure a high level of protection for human health and the environment in any event.

6.1.1 Consideration of Furnace Type

The prime function of the furnace is to achieve maximum combustion of the waste. Chapter IV of the IED requires that the plant (furnace in this context) should be designed to deliver its requirements. The main requirements of Chapter IV in relation to the choice of a furnace are compliance with air emission limits for CO and TOC and achieving a low TOC/LOI level in the bottom ash.

The Waste Incineration BREF elaborates the furnace selection criteria as:

- the use of a furnace (including secondary combustion chamber) dimensions that are large enough to provide for an effective combination of gas residence time and temperature such that combustion reactions may approach completion and result in low and stable CO and TOC emissions to air and low TOC in residues.
- use of a combination of furnace design, operation and waste throughput rate that provides sufficient agitation and residence time of the waste in the furnace at sufficiently high temperatures.
- The use of furnace design that, as far as possible, physically retain the waste within the combustion chamber (e.g. grate bar spacing) to allow its complete combustion.

The BREF also provides a comparison of combustion and thermal treatment technologies and factors affecting their applicability and operational suitability used in EU and for all types of wastes. There is also some information on the comparative costs. The table below has been extracted from the BREF tables. This table is also in line with the Guidance Note "The Incineration of

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Waste (EPR 5.01)). However, it should not be taken as an exhaustive list nor that all technologies listed have found equal application across Europe.

Overall, any of the furnace technologies listed below would be considered as BAT provided the Applicant has justified it in terms of:

- nature/physical state of the waste and its variability
- proposed plant throughput which may affect the number of incineration lines
- preference and experience of chosen technology including plant availability
- nature and quantity/quality of residues produced.
- emissions to air usually NOx as the furnace choice could have an effect on the amount of unabated NOx produced
- energy consumption whole plant, waste preparation, effect on GWP
- Need, if any, for further processing of residues to comply with TOC
- Costs

<u>Summary comparison of thermal treatment technologies</u> (reproduced from the Waste Incineration BREF)

Technique	Key waste characteristics and suitability	Throughput per line	Advantages	Disadvantages / Limitations of use	Bottom Ash Quality	Cost
Moving grate (air-cooled)	Low to medium heat values (LCV 5 – 16.5 GJ/t) Municipal and other heterogeneous solid wastes Can accept a proportion of sewage sludge and/or medical waste with municipal waste Applied at most modern MSW installations	1 to 50 t/h with most projects 5 to 30 t/h. Most industrial applications not below 2.5 or 3 t/h.	Widely proven at large scales. Robust Low maintenance cost Long operational history Can take heterogeneous wastes without special preparation	generally not suited to powders, liquids or materials that melt through the grate	TOC 0.5 % to 3 %	High capacity reduces specific cost per tonne of waste
Moving grate (liquid Cooled)	Same as air-cooled grates except: LCV 10 – 20 GJ/t	Same as air- cooled grates	As air-cooled grates but: higher heat value waste treatable better Combustion control possible.	As air-cooled grates but: risk of grate damaging leaks and higher complexity	TOC 0.5 % to 3 %	Slightly higher capital cost than air-cooled

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Technique	Key waste characteristics and suitability	Throughput per line	Advantages	Disadvantages / Limitations of use	Bottom Ash Quality	Cost
Rotary Kiln	Can accept liquids and pastes - solid feeds more limited than grate (owing to refractory damage) - often applied to hazardous wastes	<10 t/h	Very well proven with broad range of wastes and good burn out even of HW	Throughputs lower than grates	TOC <3 %	Higher specific cost due to reduced capacity
Fluid bed - bubbling	Only finely divided Consistent wastes. Limited use for raw MSW often applied to sludges	1 to 10 t/h	Good mixing Fly ashes of good leaching quality	Careful operation required to avoid clogging bed. Higher fly ash quantities.	TOC <3 %	FGT cost may be lower. Costs of waste preparation
Fluid bed - circulating	Only finely divided consistent wastes. Limited use for raw MSW, often applied to sludges / SRF.	1 to 20 t/h most used above 10 t/h	Greater fuel flexibility than BFB Fly ashes of good leaching quality	Cyclone required to conserve bed material Higher fly ash quantities	TOC <3 %	FGT cost may be lower. Costs of preparation.
Oscillating furnace	MSW / heterogeneous wastes	1 – 10 t/h	Robust Low maintenance Long history Low NOX level Low LOI of bottom ash	-higher thermal loss than with grate furnace - LCV under 15 GJ/t	TOC 0.5 – 3 %	Similar to other technologies

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Technique	Key waste characteristics and suitability	Throughput per line	Advantages	Disadvantages / Limitations of use	Bottom Ash Quality	Cost
Pulsed hearth	Only higher CV waste (LCV >20 GJ/t) used for clinical wastes	<7 t/h	can deal with liquids and powders	bed agitation may be lower	Dependen t on waste type	Higher specific cost due to reduced capacity
Stepped and static hearths	Only higher CV waste (LCV >20 GJ/t) Mainly used for clinical wastes	No information	Can deal with liquids and powders	Bed agitation may be lower	Dependen t on waste type	Higher specific cost due to reduced capacity
Spreader - stoker combustor	- SRF and other particle feeds poultry manure wood wastes	No information	- simple grate Construction less sensitive to particle size than FB	only for well defined mono-streams	No informatio n	No information
Gasification - fixed bed	- mixed plastic wastes other similar consistent streams. Gasification less widely used/proven than incineration	1 to 20 t/h	-low leaching residue good burnout if oxygen blown syngas available -Reduced oxidation of recyclable metals	 limited waste feed not full combustion high skill level tar in raw gas less widely proven 	-Low leaching bottom ash good burnout with oxygen	High operation/ maintenance costs

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Technique	Key waste characteristics and suitability	Throughput per line	Advantages	Disadvantages / Limitations of use	Bottom Ash Quality	Cost
Gasification - entrained flow	- mixed plastic wastes - other similar consistent streams -not suited to untreated MSW gasification less widely used/proven than incineration	To 10 t/h	- low leaching slag reduced oxidation of recyclable metals	- limited waste feed not full combustion high skill level less widely proven	low leaching slag	High operation/ maintenance costs pre-treatment costs high
Gasification - fluid bed	 mixed plastic wastes shredded MSW shredder residues sludges metal rich waste other similar consistent streams Less widely used/proven than incineration 	5 – 20 t/h	-temperatures e.g. for Al recovery separation of non-combustibles -can be combined with ash melting - reduced oxidation of recyclable metals	-limited waste size (<30cm) - tar in raw gas - higher UHV raw gas - less widely proven	If Combined with ash melting chamber ash is vitrified	Lower than other gasifiers
Pyrolysis	-pre-treated MSW - high metal inert streams - shredder residues/plastics - pyrolysis is less widely used/proven than incineration	~ 5 t/h (short drum) 5 – 10 t/h (medium drum)	 no oxidation of metals no combustion energy for metals/inert in reactor acid neutralisation possible syngas available 	 limited wastes process control and engineering critical high skill req. not widely proven need market for syngas 	- dependent on process temperature - residue produced requires further processing e.g. combustion	High pre- treatment, operation and capital costs

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The Applicant has carried out a review of the following candidate furnace types:

- <u>Fixed Hearth/Pulsed Hearth Furnace</u>: Fixed hearth furnaces are not considered suitable for large volumes of waste and although pulsed hearth furnaces have been used for MWI there have been reliability problems.
- Rotary Kilns: Rotary kilns have achieved good results with clinical waste, and small scale MSW plants (less than 8 tonnes per hour), but they have not been used in the UK with the same capacity of waste fuels as the proposed Installation. The energy conversion efficiency of a rotary kiln is lower than that of other waste incineration technologies due to the large areas of refractory lined combustion chamber.

The capacity per rotary or oscillating kiln unit is limited to 8 tonnes per hour. For a plant with the capacity of this application it would require more than 4 kilns to achieve the nominal design throughput for the gasification plant.

- Grate Furnaces: Grate Furnaces are designed to handle large volumes of waste fuels, such as SRF. An air cooled grate system would not be capable of processing high CV fuels such as those proposed for the Installation. Therefore, a grate furnace for the proposed fuel specification would need to be a water cooled grate. Water cooled grates typically have higher capital and maintenance costs than air cooled grates.
- <u>Pyrolysis:</u> In pyrolysis, the waste is heated in the absence of air, leading to the production of a syngas with a higher calorific value than from gasification. However, the process normally requires some form of external heat source, which may be the combustion of part of the syngas.

Pyrolysis systems are being developed for the disposal of waste fuels; however these systems are currently commercially unproven in the UK and there are no pyrolysis systems which are of a capacity required to process the nominal design capacity.

 Fluidised Bed: Fluidised beds are designed for the combustion of relatively homogeneous fuel. Therefore fluidised beds are appropriate for pretreated fuels. Where waste fuels have been pre-treated at a pre-treatment facility to produce an SRF, such as that proposed for the Installation, the pre-treated waste will already be suitable for feeding to the fluidised bed.

Fluidised bed combustion can lead to lower NOx generation however the injection of ammonia or urea is still required to achieve the relevant emission limits specified in IED.

• <u>Gasification:</u> In gasification, the waste is heated in the presence of some air, but insufficient air to achieve full combustion. This leads to the

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production of a synthetic fuel gas, or syngas, which can then be used to generate electricity. There are four different types of gasification technology:

- i) Conventional Gasification;
- ii) Plasma Gasification;
- iii) Close-coupled gasification; and
- iv) Gasification with conventional combustion.

These are considered further below.

i) Conventional Gasification

The primary benefits which are claimed for conventional gasification are higher efficiency and lower emissions.

The higher efficiency is based on the use of gas engines or gas turbines, which are more efficient at generating electricity from syngas than a conventional steam turbine is at generating electricity from steam. However, the energy used to convert waste into syngas and to clean up the syngas so that it can be used in the gas engine tends to erode this advantage, so that the overall efficiency of a gasification or pyrolysis plant tends to be similar to the overall efficiency of a conventional combustion plant.

While there are a number of suppliers offering conventional gasification technologies in the UK, and while environmental permits have been granted for such plants, there is still limited operational experience. In particular, no developer of gasification has yet managed successfully to demonstrate at a commercial scale the combination of municipal waste gasification or pyrolysis with a gas engine or gas turbine. This is because the gasification process produces tars in the syngas, which need to be removed before the syngas can be used in a gas engine.

ii) Plasma Gasification

Plasma gasification uses a high temperature electric arc furnace to break down the components of the waste fuel into a vitrified solid and low molecular weight gases. This produces a fuel gas which contains very little condensable tars and attempts to produce a synthetic gas suitable for use in a gas turbine or gas engine have not been demonstrated at commercial scale. In addition, the power consumption is very high, due to the use of high temperature and the need to make oxygen for the process.

An alternative approach is to use a fluidised bed gasifier to generate the fuel gas and then a plasma arc furnace to break down the gases into low molecular weight components. However, this process has a limited capacity and is yet to be proven in commercial operation.

iii) Close-coupled gasification

Compared to some of the other gasification technologies, this is considered to be a proven technology, as there are full-scale operational

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plants in Europe which comply with the requirements of Chapter IV of the IED.

In close-coupled gasification plants, the gasification chamber operates at a lower temperature than the combustion chamber for a conventional EfW plant. The syngas is then combusted within a separate section of the chamber to generate steam.

In close-coupled gasification, the combustion of syngas to generate steam is simpler than using other types of combustion system, as discussed above. This technology has not been considered further by Biossence, since the efficiency and power generation is no higher and potentially lower than conventional combustion technology.

iv) Gasification with conventional combustion

In this gasification process the syngas is cooled and cleaned prior to combustion within a conventional gas fired boiler. In the cleaning process, tars and particulates are removed from the syngas prior to its combustion. This means that the steam cycle can operate with higher steam conditions, giving greater efficiency for power generation than a standard close-coupled gasifier.

The process for gasifying of the incoming waste fuels will incorporate a recirculating fluidised bed. As discussed previously, fluidised bed technology is appropriate where waste fuels, such as those to be treated within the gasification plant, have been prepared at a pre-treatment facility (see item 5: Fluidised Bed Combustor).

The grate and the fluidised bed are both less efficient at generating power from the incoming fuel than the gasification system. Therefore, the gasification system has a significantly better GWP than both the grate and the fluidised bed. This is demonstrated by the fact that the gasification system will generate nearly 25% more power per tonne of waste processed than the grate or fluidised bed system.

On the basis of the above, the Applicant has given more detailed consideration to Moving Grate, Fluidised Bed and Gasification with conventional combustion technologies and has proposed to use a furnace technology comprising a circulating fluidised bed gasification process followed by combustion of the syngas in a conventional gas boiler for steam generation all of which are identified in the tables above as being considered BAT in the BREF or TGN for this type of waste feed. Further consideration of the techniques is made below:

The gasification and fluidised bed will utilise the same quantities of ammonia, where as the grate will use approximately 75% more ammonia to achieve the same NOx concentrations.

The fluidised bed and the gasification systems will produce less bottom ash than the grate, but the grate will produce slightly more APC. The fluidised bed

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will produce more boiler ash than the grate, but this ash will be non-hazardous and it may be possible for this residue to be recovered as a construction material. The gasification system will produce filter ash which will be hazardous waste.

The operating costs for the gasification system are significantly higher than a grate or a fluidised bed. This is mainly due to the disposal costs associated with the filter ash. The Power revenues for the gasification system are significantly higher for the gasification system, than both the grate and the fluidised bed, due to the ROC revenues which will be payable for a gasification system.

Due to the efficiencies associated with the gasification system and the better GWP, gasification systems are considered by the Applicant to represent BAT, irrespective of the elevated operating costs. Gasification is supported by the UK government policy through the ROC regime and ROCs are paid for the use of this technology to generate power. These technologies are considered by the Applicant to offer better environmental performance when compared to convention waste incineration technologies, such as grate or fluidised bed technologies.

On this basis, the Applicant proposes gasification with conventional combustion is considered to represent BAT for the proposed Installation.

This technology is identified in the tables above as being considered BAT in the BREF or TGN for this type of waste feed.

• The Applicant proposes to use natural gas as support fuel for start-up, shut down and for the auxiliary burners. The Applicant has justified its choice of natural gas as the support fuel on the basis that it minimises pollution and complies with the requirements of IED; "The auxiliary burner shall not be fed with fuels which can cause higher emissions than those resulting from the burning of gas oil as defined in Article 2(2) of Council Directive 1999/32/EC of 26 April 1999 relating to a reduction in the sulphur content of certain liquid fuels (1) OJ L 121, 11.5.1999, p. 13., liquefied gas or natural gas."

The Applicant confirmed in an email 14/01/15 that the supply of natural gas will be on a non interruptible basis.

We are satisfied that the use of natural gas as the fuel for the auxiliary burners represents BAT.

Boiler Design

In accordance with our Technical Guidance Note, S5.01, the Applicant has confirmed that the boiler design will include the following features to minimise the potential for reformation of dioxins within the de-novo synthesis range:

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- ensuring that the steam/metal heat transfer surface temperature is a minimum where the exhaust gases are within the de-novo synthesis range;
- design of the boilers using CFD to ensure no pockets of stagnant or low velocity gas;
- boiler passes are progressively decreased in volume so that the gas velocity increases through the boiler; and
- Design of boiler surfaces to prevent boundary layers of slow moving gas.

We have considered the assessments made by the Applicant and agree that the furnace technology chosen represents BAT. We believe that, based on the information gathered by the BREF process, the chosen technology will achieve the requirements of Chapter IV of the IED for the air emission of TOC/CO and the TOC on bottom ash.

However we have included pre-operational condition P05 that requires the Applicant to submit a report providing details and conclusions from the CFD modelling design study for the specified combustion unit and boiler system design that has been selected for the plant.

6.2 BAT and emissions control

The prime function of flue gas treatment is to reduce the concentration of pollutants in the exhaust gas as far as practicable. The techniques which are described as BAT individually are targeted to remove specific pollutants, but the BREF notes that there is benefit from considering the FGT system as a whole unit. Individual units often interact, providing a primary abatement for some pollutants and an additional effect on others.

The BREF lists the general factors requiring consideration when selecting flue-gas treatment (FGT) systems as:

- type of waste, its composition and variation
- type of combustion process, and its size
- flue-gas flow and temperature
- flue-gas content, size and rate of fluctuations in composition
- target emission limit values
- restrictions on discharge of aqueous effluents
- plume visibility requirements
- land and space availability
- availability and cost of outlets for residues accumulated/recovered
- compatibility with any existing process components (existing plants)
- availability and cost of water and other reagents
- energy supply possibilities (e.g. supply of heat from condensing scrubbers)
- reduction of emissions by primary methods
- release of noise.

Taking these factors into account the Technical Guidance Note points to a range of technologies being BAT subject to circumstances of the Installation.

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6.2.1 Particulate Matter

Particulate matter							
Technique	Advantages	Disadvantages	Optimisation	Defined as BAT in BREF or TGN for:			
Bag/Fabric filters (BF)	Reliable abatement of particulate matter to below 5mg/m ³	Max temp 250°C	Multiple compartments Bag burst detectors	Most plants			
Wet scrubbing	May reduce acid gases simultaneously.	Not normally BAT. Liquid effluent produced	Require reheat to prevent visible plume and dew point problems.	Where scrubbing required for other pollutants			
Ceramic filters	High temperature applications Smaller plant.	May "blind" more than fabric filters		Small plant. High temperature gas cleaning required.			
Electrostatic precipitators	Low pressure gradient. Use with BF may reduce the energy consumption of the induced draft fan.	Not normally BAT.		When used with other particulate abatement plant			

The Applicant proposes to use fabric filters for the abatement of particulate matter. Fabric filters provide reliable abatement of particulate matter to below 5 mg/m³ and are BAT for most installations. The Applicant proposes to use multiple compartment filters with burst bag detection to minimise the risk of increased particulate emissions in the event of bag rupture.

Emissions of particulate matter have been previously assessed as insignificant, and so the Environment Agency agrees that the Applicant's proposed technique is BAT for the Installation.

6.2.2 Oxides of Nitrogen

Oxides of Nitrogen : Primary Measures				
Technique	Advantages	Disadvantages	Optimisation	Defined as BAT in BREF or TGN for:
Low NO burners	Reduces NOx at source		Start-up, supplementary firing.	Where auxiliary burners

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			required.
Starved air	Reduce CO		Pyrolysis,
systems	simultaneously.		Gasification
			systems.
Optimise			All plant.
primary and			
secondary air			
injection			
Flue Gas	Reduces the	Some	All plant
Recirculation	consumption of	applications	unless
(FGR)	reagents used	experience	impractical in
	for secondary	corrosion	design (needs
	NOx control.	problems.	to be
			demonstrated)
	May increase		
	overall energy		
	recovery		

Oxides of Nitro	ogen : Secondar	y Measures (BAT	is to apply Pri	mary Measures
Technique	Advantages	Disadvantages	Optimisation	Defined as BAT in BREF or TGN for:
Selective catalytic reduction (SCR)	NOx emissions < 70mg/ m³ Reduces CO, VOC, dioxins	Re-heat required – reduces plant efficiency		All plant
Selective non-catalytic reduction (SNCR)	NOx emissions typically 150 - 180mg/m ³	Relies on an optimum temperature around 900 °C, and sufficient retention time for reduction May lead to Ammonia slip	Port injection location	All plant unless lower NOx release required for local environmental protection.
Reagent Type: Ammonia	Likely to be BAT Lower nitrous oxide formation	More difficult to handle Narrower temperature window		All plant
Reagent Type: Urea	Likely to be BAT			All plant

The Applicant proposes to implement the following primary measures:

ullet Low NO_x burners – this technique reduces NO_x at source and is defined as BAT where auxiliary burners are required.

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- Optimise primary and secondary air injection this technique is BAT for all plant.
- Flue Gas Recirculation (FGR) Flue Gas Recirculation has been rejected based on the specific technology choice design and compensated with the choice of the optimum secondary BAT SCR abatement as discussed below. The operator stated that FGR was rejected due to the need for stable flame control. The operator argued that the FGR dilutes the syngas and creates flame control problems which result in unstable operation and the possibility of uncontrolled emissions. Under such conditions the technology operator would not be able to guarantee the thermal conversion conditions of 2 seconds residence time at 850°C. FGR was therefore rejected.
- Starved air systems Starved air systems are not considered appropriate for this specific combustion technology as they can affect flame stability. Starving the gas boiler furnace of combustion air to reduce oxygen content and temperature in the area of the low NOx syngas burners creates flame control problems which results in unstable operations and the possibility of abnormal emissions to atmosphere.

There are two recognised techniques for secondary measures to reduce NO_x . These are Selective Catalytic Reduction (SCR) and Selective Non-Catalytic Reduction (SNCR). For each technique, there is a choice of urea or ammonia reagent.

SCR can reduce NO_x levels to below 70 mg/m³ and can be applied to all plant, it is generally more expensive than SNCR and requires reheating of the waste gas stream which reduces energy efficiency, periodic replacement of the catalysts also produces a hazardous waste. SNCR can typically reduce NO_x levels to between 150 and 180 mg/m³, it relies on an optimum temperature of around 900 deg C and sufficient retention time for reduction. SNCR is more likely to have higher levels of ammonia slip. The technique can be applied to all plant unless lower NO_x releases are required for local environmental protection. Urea or ammonia can be used as the reagent with either technique, urea is somewhat easier to handle than ammonia and has a wider operating temperature window, but tends to result in higher emissions of N_2O . Either reagent is BAT, and the use of one over the other is not normally significant in environmental terms.

The Applicant proposes to use SCR with ammonia solution as the reagent. The use of SNCR has not been considered as an SNCR system would not be able to achieve the reduced NOx emissions proposed by the Applicant. The Environment Agency agrees with this assessment.

Emissions of NO_x cannot be screened out as insignificant however by using SCR as the abatement technique emissions have been assessed as being unlikely to give rise to significant pollution in that the predicted environmental concentration is less than 100%.

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The amount of ammonia used for NO_x abatement will need to be optimised to maximise NO_x reduction and minimise NH_3 slip. Improvement condition IC4 requires the Operator to report to the Environment Agency on optimising the performance of the NO_x abatement system. The Operator is also required to monitor and report on NH_3 and N_2O emissions every 6 months.

6.2.3 Acid Gases, SO_x, HCl and HF

Acid gases and	d halogens : Prim	nary Measures		
Technique	Advantages	Disadvantages	Optimisation	Defined as BAT in BREF or TGN for:
Low sulphur fuel, (< 0.1%S gasoil or natural gas)	Reduces SOx at source		Start-up, supplementary firing.	Where auxiliary fuel required.
Management of waste streams	Disperses sources of acid gases (e.g. PVC) through feed.	Requires closer control of waste management		All plant with heterogeneous waste feed

Acid gases ar Measures first)		Secondary Measu	ires (BAT is to	apply Primary
Technique	Advantages	Disadvantages	Optimisation	Defined as BAT in BREF or TGN for:
Wet	High reaction rates Low solid	Large effluent disposal and water consumption		Plants with high acid gas and metal components
	residues production	if not fully treated for re- cycle		in exhaust gas – HWIs
	Reagent delivery may be optimised by concentration	Effluent treatment plant required		
	and flow rate	May result in wet plume		
		Energy required for effluent treatment and plume reheat		
Dry	Low water use	Higher solid residue production		All plant

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	Reagent consumption may be reduced by recycling in plant Lower energy use	Reagent consumption controlled only by input rate		
	Higher reliability			
Semi-dry	Medium reaction rates Reagent delivery may be varied by	Higher solid waste residues		All plant
	concentration and input rate			
Reagent Type: Sodium Hydroxide	Highest removal rates Low solid waste production	Corrosive material ETP sludge for disposal		HWIs
Reagent Type: Lime	Very good removal rates Low leaching solid residue Temperature of reaction well suited to use with bag filters	Corrosive material May give greater residue volume if no in-plant recycle	Wide range of uses	MWIs, CWIs
Reagent Type: Sodium Bicarbonate	Good removal rates Easiest to handle Dry recycle systems proven	Efficient temperature range may be at upper end for use with bag filters Leachable solid residues	Not proven at large plant	CWIs

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Bicarbonate	
more	
expensive	

The Applicant proposes to implement the following primary measures:

- Use of low sulphur fuels for start up and auxiliary burners gas should be used if available, where fuel oil is used, this will be low sulphur (i.e. <0.1%), this will reduce SO_x at source. The Applicant has justified its choice of gas as the support fuel on the basis that it minimises pollution and we agree with that assessment.
- Management of heterogeneous wastes the Applicant proposes to use SRF; this will ensure a homogeneous waste feed removing the risk of problem wastes such as PVC affecting emissions.

There are three recognised techniques for secondary measures to reduce acid gases. These are wet, dry and semi-dry. Wet scrubbing produces an effluent for treatment and disposal in compliance with Article 46(3) of IED. It will also require reheat of the exhaust to avoid a visible plume. Wet scrubbing is unlikely to be BAT except where there are high acid gas and metal components in the exhaust gas as may be the case for some hazardous waste incinerators. In this case, the Applicant does not propose using wet scrubbing, and the Environment Agency agrees that wet scrubbing is not appropriate in this case.

The Applicant has therefore considered dry and semi-dry methods of secondary measures for acid gas abatement. Either can be BAT for this type of facility.

Both dry and semi-dry methods rely on the dosing of powdered materials into the exhaust gas stream. Semi-dry systems (i.e. hydrated reagent) offer reduced material consumption through faster reaction rates, but reagent recycling in dry systems can offset this.

In both dry and semi-dry systems, the injected powdered reagent reacts with the acid gases and is removed from the gas stream by the bag filter system. The powdered materials are either lime or sodium bicarbonate. Both are effective at reducing acid gases, and dosing rates can be controlled from continuously monitoring acid gas emissions. The decision on which reagent to use is normally economic. Lime produces a lower leaching solid residue in the APC residues than sodium bicarbonate and the reaction temperature is well suited to bag filters, it tends to be lower cost, but it is a corrosive material and can generate a greater volume of solid waste residues than sodium bicarbonate. Either reagent is BAT, and the use of one over the other is not significant in environmental terms in this case.

The Applicant considered the methods and concluded that the performance of the two options is very similar. Whilst the dry system is slightly preferable from an economic perspective, the semi-dry system has a lower global warming potential and generates slightly less hazardous waste

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In this case, the Applicant proposes to use the semi-dry system due to the lower global warming potential and the generation of less hazardous waste. The Environment Agency is satisfied that this is BAT

6.2.4 Carbon monoxide and volatile organic compounds (VOCs)

The prevention and minimisation of emissions of carbon monoxide and volatile organic compounds is through the optimisation of combustion controls, where all measures will increase the oxidation of these species.

Carbon monox	ide and volatile o	rganic compoun	ds (VOCs)	
Technique	Advantages	Disadvantages	Optimisation	Defined as BAT in BREF or TGN for:
Optimise combustion	All measures will increase		Covered in section on	All plants
control	oxidation of these species.		furnace selection	

6.2.5 <u>Dioxins and furans (and Other POPs)</u>

Dioxins and fu	rans			
Technique	Advantages	Disadvantages	Optimisation	Defined as BAT in BREF or TGN for:
Optimise combustion control	All measures will increase oxidation of these species.		Covered in section on furnace selection	All plants
Avoid de novo synthesis			Covered in boiler design	All plant
Effective Particulate matter removal			Covered in section on particulate matter	All plant
Activated Carbon injection	Can be combined with acid gas absorber or fed separately.	Combined feed rate usually controlled by acid gas content.		All plant. Separate feed normally BAT unless feed is constant and acid gas control also controls dioxin release.

The prevention and minimisation of emissions of dioxins and furans is achieved through:

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- optimisation of combustion control including the maintenance of permit conditions on combustion temperature and residence time, which has been considered in 6.1.1 above;
- avoidance of de novo synthesis, which has been covered in the consideration of boiler design;
- the effective removal of particulate matter, which has been considered in 6.2.1 above:
- injection of activated carbon. This can be combined with the acid gas reagent or dosed separately. Where the feed is combined, the combined feed rate will be controlled by the acid gas concentration in the exhaust. Therefore, separate feed of activated carbon would normally be considered BAT unless the feed was relatively constant. Effective control of acid gas emissions also assists in the control of dioxin releases.

In this case the Applicant proposes separate feed and we are satisfied their proposals are BAT.

6.2.6 Metals

Metals				
Technique	Advantages	Disadvantages	Optimisation	Defined as BAT in BREF or TGN for:
Effective Particulate matter removal			Covered in section on particulate matter	All plant
Activated Carbon injection for mercury recovery	Can be combined with acid gas absorber or fed separately.	Combined feed rate usually controlled by acid gas content.		All plant. Separate feed normally BAT unless feed is constant and acid gas control also controls dioxin release.

The prevention and minimisation of metal emissions is achieved through the effective removal of particulate matter, and this has been considered in 6.2.1 above.

Unlike other metals however, mercury if present will be in the vapour phase. BAT for mercury removal is also dosing of activated carbon into the exhaust gas stream. This can be combined with the acid gas reagent or dosed separately. Where the feed is combined, the combined feed rate will be controlled by the acid gas concentration in the exhaust. Therefore, separate feed of activated carbon would normally be considered BAT unless the feed was relatively constant.

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In this case the Applicant proposes separate feed and we are satisfied their proposals are BAT.

6.3 BAT and global warming potential

This section summarises the assessment of greenhouse gas impacts which has been made in the determination of this Permit. Emissions of carbon dioxide (CO_2) and other greenhouse gases differ from those of other pollutants in that, except at gross levels, they have no localised environmental impact. Their impact is at a global level and in terms of climate change. Nonetheless, CO_2 is clearly a pollutant for IED purposes.

The principal greenhouse gas emitted is CO_2 , but the plant also emits small amounts of N_2O arising from the operation of secondary NO_x abatement. N_2O has a global warming potential 310 times that of CO_2 . The Applicant will therefore be required to optimise the performance of the secondary NO_x abatement system to ensure its GWP impact is minimised.

The major source of greenhouse gas emissions from the installation is however CO_2 from the combustion of waste. There will also be CO_2 emissions from the burning of support fuels at start up, shut down and should it be necessary to maintain combustion temperatures. BAT for greenhouse gas emissions is to maximise energy recovery and efficiency.

The electricity that is generated by the Installation will displace emissions of CO₂ elsewhere in the UK, as virgin fossil fuels will not be burnt to create the same electricity.

The Installation is not subject to the Greenhouse Gas Emissions Trading Scheme Regulations 2012 therefore it is a requirement of IED to investigate how emissions of greenhouse gases emitted from the installation might be prevented or minimised.

Factors influencing GWP and CO_2 emissions from the Installation are: On the debit side

- CO₂ emissions from the burning of the waste;
- CO₂ emissions from burning auxiliary or supplementary fuels;
- CO₂ emissions associated with electrical energy used;
- N₂O from the de-NOx process.

On the credit side

 CO₂ saved from the export of electricity to the public supply by displacement of burning of virgin fuels;

Note: avoidance of methane which would be formed if the waste was landfilled has not been included in this assessment. If it were included due to its avoidance it would be included on the credit side. Ammonia has no direct GWP effect.

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The GWP of the plant will be dominated by the emissions of carbon dioxide that are released as a result of waste combustion. This will be constant for all options considered in the BAT assessment. Any differences in the GWP of the options in the BAT appraisal will therefore arise from small differences in energy recovery and in the amount of N_2O emitted.

The Applicant considered energy efficiency and compared SCR to SNCR in its BAT assessment. This is set out in sections 4.3.7, 6.1.1 and 6.2.2 of this decision document.

Taking all these factors into account, the Operator's assessment shows their preferred option is best in terms of GWP.

The Environment Agency agrees with this assessment and that the chosen option is BAT for the installation.

6.4 BAT and POPs

International action on Persistent Organic pollutants (POPs) is required under the UN's Stockholm Convention, which entered into force in 2004. The EU implemented the Convention through the POPs Regulation (850/2004), which is directly applicable in UK law. The Environment Agency is required by national POPs Regulations (SI 2007 No 3106) to give effect to Article 6(3) of the EC POPs Regulation when determining applications for environmental Permits.

However, it needs to be borne in mind that this application is for a particular type of installation, namely a waste incinerator. The Stockholm Convention distinguishes between intentionally-produced and unintentionally-produced POPs. Intentionally-produced POPs are those used deliberately (mainly in the past) in agriculture (primarily as pesticides) and industry. Those intentionally-produced POPs are not relevant where waste incineration is concerned, as in fact high-temperature incineration is one of the prescribed methods for destroying POPs.

The unintentionally-produced POPs addressed by the Convention are:

- dioxins and furans;
- HCB (hexachlorobenzene)
- PCBs (polychlorobiphenyls) and
- PeCB (pentachlorobenzene)

The UK's national implementation plan for the Stockholm Convention, published in 2007, makes explicit that the relevant controls for unintentionally-produced POPs, such as might be produced by waste incineration, are delivered through the requirements of IED. That would include an examination of BAT, including potential alternative techniques, with a view to preventing or minimising harmful emissions. These have been applied as explained in this document, which explicitly addresses alternative techniques and BAT for the minimisation of emissions of dioxins.

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Our legal obligation, under regulation 4(b) of the POPs Regulations, is, when considering an application for an environmental permit, to comply with article 6(3) of the POPs Regulation:

"Member States shall, when considering proposals to construct new facilities or significantly to modify existing facilities using processes that release chemicals listed in Annex III, without prejudice to Council Directive 1996/61/EC, give priority consideration to alternative processes, techniques or practices that have similar usefulness but which avoid the formation and release of substances listed in Annex III."

The 1998 Protocol to the Convention recommended that unintentionally produced should be controlled by imposing emission limits (e.g. 0.1 ng/m³ for MWIs) and using BAT for incineration. UN Economic Commission for Europe (Executive Body for the Convention) (ECE-EB) produced BAT guidance for the parties to the Convention in 2009. This document considers various control techniques and concludes that primary measures involving management of feed material by reducing halogenated substances are not technically effective. This is not surprising because halogenated wastes still need to be disposed of and because POPs can be generated from relatively low concentrations of halogens. In summary, the successful control techniques for waste incinerators listed in the ECE-EB BAT are:

- maintaining furnace temperature of 850°C and a combustion gas residence time of at least 2 seconds
- rapid cooling of flue gases to avoid the *de novo* reformation temperature range of 250-450°C
- use of bag filters and the injection of activated carbon or coke to adsorb residual POPs components.

Using the methods listed above, the UN-ECE BAT document concludes that incinerators can achieve an emission concentration of 0.1 ng TEQ/m³.

We believe that the Permit ensures that the formation and release of POPs will be prevented or minimised. As we explain above, high-temperature incineration is one of the prescribed methods for destroying POPs. Permit conditions are based on the use of BAT and Chapter IV of IED and incorporate all the above requirements of the UN-ECE BAT guidance and deliver the requirements of the Stockholm Convention in relation to unintentionally produced POPs.

The release of **dioxins and furans** to air is required by the IED to be assessed against the I-TEQ (International Toxic Equivalence) limit of 0.1 ng/m³. Further development of the understanding of the harm caused by dioxins has resulted in the World Health Organisation (WHO) producing updated factors to calculate the WHO-TEQ value. Certain **PCBs** have structures which make them behave like dioxins (dioxin-like PCBs), and these also have toxic equivalence factors defined by WHO to make them capable of being considered together with dioxins. The UK's independent health advisory committee, the Committee on Toxicity of Chemicals in Food, Consumer Products and the Environment (COT) has adopted WHO-TEQ

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values for both dioxins and dioxin-like PCBs in their review of Tolerable Daily Intake (TDI) criteria. In support of the requirements of the IED, the WHO-TEQ values for both dioxins and dioxin-like PCBs have been specified for monitoring and reporting purposes, to enable an evaluation of exposure to dioxins and dioxin-like PCBs to be made using the revised TDI recommended by COT. The release of dioxin-like PCBs and PAHs is expected to be low where measures have been taken to control dioxin releases. We specify monitoring of a range of PAHs and dioxin-like PCBs in waste incineration Permits at the same frequency as dioxins are monitored. We have included a requirement to monitor and report against these WHO-TEQ values for dioxins and dioxin-like PCBs and the range of PAHs identified by Defra in their previous Environmental Permitting Guidance on the WID. We are confident that the measures taken to control the release of dioxins will also control the releases of dioxin-like PCBs and PAHs. Section 5.2 of this document details the assessment of emissions to air, which includes dioxins and concludes that there will be no adverse effect on human health from either normal or abnormal operation.

Hexachlorobenzene (HCB) is released into the atmosphere as an accidental product from the combustion of coal, waste incineration and certain metal processes. It has also been used as a fungicide, especially for seed treatment although this use has been banned in the UK since 1975. Natural fires and volcanoes may serve as natural sources. Releases of (HCB) are addressed by the European Environment Agency (EEA), which advises that:

"due to comparatively low levels in emissions from most (combustion) processes special measures for HCB control are usually not proposed. HCB emissions can be controlled generally like other chlorinated organic compounds in emissions, for instance dioxins/furans and PCBs: regulation of time of combustion, combustion temperature, temperature in cleaning devices, sorbents application for waste gases cleaning etc." [reference http://www.eea.europa.eu/publications/EMEPCORINAIR4/sources_of-HCB.pdf]

Pentachlorobenzene (PeCB) is another of the POPs list to be considered under incineration. PeCB has been used as a fungicide or flame retardant, there is no data available however on production, recent or past, outside the UN-ECE region. PeCBs can be emitted from the same sources as for PCDD/F: waste incineration, thermal metallurgic processes and combustion plants providing energy. As discussed above, the control techniques described in the UN-ECE BAT guidance and included in the permit, are effective in controlling the emissions of all relevant POPs including PeCB.

We have assessed the control techniques proposed for dioxins by the Applicant and have concluded that they are appropriate for dioxin control. We are confident that these controls are in line with the UN-ECE BAT guidance and will minimise the release of HCB, PCB and PeCB.

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We are therefore satisfied that the substantive requirements of the Convention and the POPs Regulation have been addressed and complied with.

6.5 Other Emissions to the Environment

6.5.1 Emissions to water

There will not be any process discharges to water from the installation.

Surface water run-off from roads, vehicle parking areas, building roofs, hardstandings and hard landscaped areas will be discharged into a Balancing Pond which will discharge uncontaminated rainwater to the Manchester Ship Canal via emission point W1. Discharges from roads, car parks, areas of hardstanding and paved areas which could be potentially contaminated by oils will be discharged into the Balancing Pond via a Class 1 Bypass oil interceptor.

Based upon the information in the application we are satisfied that appropriate measures will be in place to prevent and /or minimise emissions to water.

6.5.2 Emissions to sewer

There will be small quantities of process water, such as boiler blowdown and effluent from the demineralised water system, this will be discharged to sewer in accordance with a Trade Effluent Consent from the installation via emission point S1.

An application for the Trade Effluent Consent will submitted to the sewerage undertaker following completion of detailed design.

Based upon the information in the application we are satisfied that appropriate measures will be in place to prevent and /or minimise emissions to sewer.

6.5.3 Fugitive emissions

The IED specifies that plants must be able to demonstrate that the plant is designed in such a way as to prevent the unauthorised and accidental release of polluting substances into soil, surface water and groundwater. In addition storage requirements for waste and for contaminated water of Article 46(5) must be arranged.

The Applicant has provided a risk assessment and management plan for fugitive emissions, which the Environment Agency considers to be satisfactory and should ensure compliance with permit conditions, specifically condition 3.3.

The facility includes a back up diesel emergency generator to provide electrical power to safely shut down the incinerator in the event of the non availability of electrical power.

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Each storage silo used for hydrated lime, activated carbon and APC residues will be fitted with filters to prevent fugitive releases during loading/unloading.

Aqueous ammonia will be delivered in sealed tankers and off-loaded via a standard hose connection into a tank within a bunded area. Vapour displaced from the storage tank during unloading will be vented into delivery tanker.

Other measures regarding the protection of land, surface water and groundwater at the site are recorded in section 4.2.2 above.

Based upon the information in the application we are satisfied that appropriate measures will be in place to prevent and /or minimise fugitive emissions.

6.5.4 Odour

The system is designed so that air will be extracted from potentially odorous areas for combustion within the Syngas Boiler. The high temperatures will destroy any odours prior to release via the stack.

Unloading stations will have a 'foul air system. This will duct air extracted from the waste unloading areas to the gasification process to provide combustion air.

Conveyors for the transfer of fuel from the unloading areas to the storage silos and gasification process are enclosed to minimise the potential for odour.

The main fuel storage silos will be maintained under slight negative pressure, to ensure that no odours are able to escape and will be operated on a first-in first-out basis, which will prevent the fuel within the storage silos putrefying.

Air will be extracted by a fan from the fuel day storage silos and will pass through a filter prior to release at a height of 44m - 3m above the gasifier hall roof.

During periods of planned shutdown, the fuel storage silos will be emptied while the system runs down.

During extended periods of unplanned shutdown, the silos will be manually emptied as soon as possible, and fuel will be transferred off-site. The extraction fan and filter will continue to be in operation using back-up power sources to maintain the negative pressure.

A Schedule 5 notice was issued requesting more detailed information on the specification of the waste derived fuel and systems to minimise odour. The responses received dated 09/07/15 and 02/09/15 clarified that the fuel would be SRF produced to the CEN 15359: 2011 standard and provided further

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information with respect to waste acceptance procedures (document titled Environment Agency: Hooton Feedstock Quality Management Procedures).

In addition pre-operational conditions PO 08 and PO 09 are included requiring the provision of an approved Odour Management Plan and formal documented procedures for the preventative inspection and subsequent maintenance of all process items that pose a potential nuisance risk through odour. A further pre-operational condition PO 10 requires the Operator to submit to the Environment Agency for approval the final design for the fuel storage area and procedures for the removal of unacceptable waste.

Based upon the information in the application we are satisfied that the appropriate measures will be in place to prevent or where that is not practicable to minimise odour and to prevent pollution from odour.

6.5.5 Noise and vibration

Based upon the information in the application we are satisfied that the appropriate measures will be in place to prevent or where that is not practicable to minimise noise and vibration and to prevent pollution from noise and vibration outside the site.

The application contained a noise impact assessment which identified local noise-sensitive receptors, potential sources of noise at the proposed plant and noise attenuation measures. Measurements were taken of the prevailing ambient noise levels to produce a baseline noise survey and an assessment was carried out to compare the predicted plant rating noise levels with the established background levels. The applicant has not completed a BS4142 assessment. However, they have included numerical predictions at appropriate receptors and provided background values which enable BS4142 conclusions to be made.

We have completed check modelling and sensitivity analysis. Based on our sensitivity analysis our predictions are only slightly higher than those presented by the applicant. Applying the higher predictions as a reasonable worst-case is an indicative BS4142 assessment which shows that impacts at all receptors are likely to be below the level indicating marginal significance. We are therefore satisfied that the applicant's predicted values can be used for determination purposes.

Our interpretation of the applicant's model and based on our check modelling, allow us to conclude that the impacts are likely to be below the level indicating marginal significance.

6.6 Setting ELVs and other Permit conditions

6.6.1 Translating BAT into Permit conditions

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Article 14(3) of IED states that BAT conclusions shall be the reference for permit conditions. Article 15(3) further requires that under normal operating conditions; emissions do not exceed the emission levels associated with the best available techniques as laid down in the decisions on BAT conclusions.

At the time of writing of this document, no BAT conclusions have been published for waste incineration or co-incineration.

The use of IED Chapter IV emission limits for air dispersion modelling sets the worst case scenario. If this shows emissions are insignificant then we have accepted that the Applicant's proposals are BAT, and that there is no justification to reduce ELVs below the Chapter IV limits in these circumstances.

Below we consider whether, for those emission not screened out as insignificant, different conditions are required as a result of consideration of local or other factors, so that no significant pollution is caused (Article 11(c)) or to comply with environmental quality standards (Article 18).

(i) Local factors

We have considered the impact on local receptors and habitat conservation sites for those emissions not screened out as insignificant and do not consider it necessary to impose further conditions. The applicant has confirmed that emissions of NOx will be less than 100 mg/m³ and we have therefore set more stringent emission limits than those specified by IED.

(ii) National and European EQSs

We have considered the impact on local receptors and habitat conservation sites for those emissions not screened out as insignificant and do not consider it necessary to impose further conditions, or set more stringent emission limits than those specified by IED.

(iii) Global Warming

 ${\rm CO_2}$ is an inevitable product of the combustion of waste. The amount of ${\rm CO_2}$ emitted will be essentially determined by the quantity and characteristics of waste being incinerated, which are already subject to conditions in the Permit. It is therefore inappropriate to set an emission limit value for ${\rm CO_2}$, which could do no more than recognise what is going to be emitted. The gas is not therefore targeted as a key pollutant under Annex II of IED, which lists the main polluting substances that are to be considered when setting emission limit values (ELVs) in Permits.

We have therefore considered setting equivalent parameters or technical measures for CO₂. However, provided energy is recovered efficiently (see section 4.3.7 above), there are no additional equivalent technical measures (beyond those relating to the quantity and characteristics of the waste) that

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can be imposed that do not run counter to the primary purpose of the plant, which is the destruction of waste. Controls in the form of restrictions on the volume and type of waste that can be accepted at the Installation and permit conditions relating to energy efficiency effectively apply equivalent technical measures to limit CO₂ emissions.

(iv) Commissioning

Before the plant can become fully operational it will be necessary for it to be commissioned. Before commissioning can commence the Operator is required by pre-operational condition PO3 to submit a commissioning plan to the Agency for approval. Commissioning can only begin and be carried out in accordance with the approved proposals in the plan.

In addition, it is recognised that certain information presented in the Application was based on design data, or data from comparable equipment, the commissioning phase is the earliest opportunity to verify much of this information. The following improvement conditions have been included in the permit so that appropriate verifications will be determined by the Applicant:

- Calibration of CEMs in accordance with BS EN 14181 (a requirement in improvement condition IC6).
- Verification of furnace residence time, temperature and oxygen content (IC3).
- The plant in total conforms with the permit conditions and that satisfactory process control procedures for the plant have been developed (IC2).
- Abatement plant optimisation details (IC4).

6.7 Monitoring

6.7.1 Monitoring during normal operations

We have decided that monitoring should be carried out for the parameters listed in Schedule 3 using the methods and to the frequencies specified in those tables. These monitoring requirements have been imposed in order to demonstrate compliance with emission limit values and to enable correction of measured concentration of substances to the appropriate reference conditions; to gather information about the performance of the SCR system; to establish data on the release of dioxin-like PCBs and PAHs from the incineration process and to deliver the requirements of Chapter IV of IED for monitoring of residues and temperature in the combustion chamber.

Within this permit application the Applicant requested a relaxation of the requirement to continuously monitor hydrogen fluoride (HF).

Part 6, 2.3 of the IED allows that if equipment is in place which is able to control hydrogen chloride (HCl) emissions below the HCl ELV and continuously monitor HCl (to MCERTS standards) then the requirement to continuously monitor HF is removed.

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In the CEMS proposed, the Operator will be able to continuously monitor HCl to MCERTS standards and the use of a caustic scrubber with pH control in the flue gas treatment train satisfies the criterion of maintaining HCl emissions below the ELV.

We agree with the Operators proposals and therefore remove the need to continuously monitor for HF replacing it with the requirement to sample and monitor HF content quarterly in first year then on a 6-monthly frequency.

For emissions to air, the methods for continuous and periodic monitoring are in accordance with the Environment Agency's Guidance M2 for monitoring of stack emissions to air.

Based on the information in the Application and the requirements set in the conditions of the permit we are satisfied that the Operator's techniques, personnel and equipment will have either MCERTS certification or MCERTS accreditation as appropriate.

6.7.2 <u>Monitoring under abnormal operations arising from the failure of the installed CEMs</u>

The Operator has stated that they will provide back-up CEMS working in parallel to the operating CEMS. These will be switched into full operation immediately in the event that there is any failure in the regular monitoring equipment. The back-up CEMS measure the same parameters as the operating CEMS. In the unlikely event that the back-up CEMS also fail Condition 2.3.10 of the permit requires that the abnormal operating conditions apply.

6.7.3 Continuous emissions monitoring for dioxins and heavy metals

Chapter IV of IED specifies manual extractive sampling for heavy metals and dioxin monitoring. However, Article 48(5) of the IED enables The Commission to act through delegated, authority to set the date from which continuous measurements of the air emission limit values for heavy metals, dioxins and furans shall be carried out, as soon as appropriate measurement techniques are available within the Community. No such decision has yet been made by the Commission.

The Environment Agency has reviewed the applicability of continuous sampling and monitoring techniques to the installation.

Recent advances in mercury monitoring techniques have allowed standards to be developed for continuous mercury monitoring, including both vapour-phase and particulate mercury. There is a standard which can apply to CEMs which measure mercury (EN 15267-3) and standards to certify CEMs for mercury, which are EN 15267-1 and EN 15267-3. Furthermore, there is an MCERTS-

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certified CEM which has been used in trials in the UK and which has been verified on-site using many parallel reference tests as specified using the steps outlined in EN 14181.

In the case of dioxins, equipment is available for taking a sample for an extended period (several weeks), but the sample must then be analysed in the conventional way. However, the continuous sampling systems do not meet the requirements of BS EN 1948 which is the standard for dioxin analysis. BS EN 1948 requires traversing the sampler across the duct and collecting parts of the sample at various points across the duct to ensure that all of the gas phase is sampled proportionately, in case there are variations in gas flow rate or composition resulting in a non-homogeneous gas flow. This requirement is particularly important where suspended solids are present in the gas, and dioxins are often associated with suspended solid particles. Continuous samplers are currently designed for operation at one or two fixed sampling points within the duct, and traverses are not carried out automatically. Using such samplers, more information could be obtained about the variation with time of the dioxin measurement, but the measured results could be systematically higher or lower than those obtained by the approved standard method which is the reference technique required to demonstrate compliance with the limit specified in the IED. The lack of a primary reference method (e.g. involving a reference gas of known concentration of dioxin) prohibits any one approach being considered more accurate than another. Because compliance with the IED's requirements is an essential element of EPR regulation, we have set emission limits for dioxins in the permit based on the use of BS EN 1948 and the manual sampling method remains the only acceptable way to monitor dioxins for the purpose of regulation.

For either continuous monitoring of mercury or continuous sampling of dioxins to be used for regulatory purposes, an emission limit value would need to be devised which is applicable to continuous monitoring. Such limits for mercury and dioxins have not been set by the European Commission. Use of a manual sample train is the only technique which fulfils the requirements of the IED. At the present time, it is considered that in view of the predicted low levels of mercury and dioxin emission it is not justifiable to require the Operator to install additionally continuous monitoring or sampling devices for these substances.

In accordance with its legal requirement to do so, the Environment Agency reviews the development of new methods and standards and their performance in industrial applications. In particular the Environment Agency considers continuous sampling systems for dioxins to have promise as a potential means of improving process control and obtaining more accurate mass emission estimates.

6.8 Reporting

We have specified the reporting requirements in Schedule 5 of the Permit either to meet the reporting requirements set out in the IED, or to ensure data is reported to enable timely review by the Environment Agency to ensure

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7 Other legal requirements

In this section we explain how we have addressed other relevant legal requirements, to the extent that we have not addressed them elsewhere in this document.

7.1 The EPR 2010 and related Directives

The EPR delivers the requirements of a number of European and national laws.

7.1.1 Schedules 1 and 7 to the EPR 2010 – **IED Directive**

We address the requirements of the IED in the body of this document above and the specific requirements of Chapter IV in Annex 1 of this document.

There is one requirement not addressed above, which is that contained in Article 5(3) IED. Article 5(3) requires that "In the case of a new installation or a substantial change where Article 4 of Directive 85/337/EC (the EIA Directive) applies, any relevant information obtained or conclusion arrived at pursuant to articles 5, 6 and 7 of that Directive shall be examined and used for the purposes of granting the permit."

- Article 5 of EIA Directive relates to the obligation on developers to supply the information set out in Annex IV of the Directive when making an application for development consent.
- Article 6(1) requires Member States to ensure that the authorities likely to be concerned by a development by reason of their specific environmental responsibilities are consulted on the Environmental Statement and the request for development consent.
- Article 6(2)-6(6) makes provision for public consultation on applications for development consent.
- Article 7 relates to projects with transboundary effects and consequential obligations to consult with affected Member States.

The grant or refusal of development consent is a matter for the relevant local planning authority. The Environment Agency's obligation is therefore to examine and use any relevant information obtained or conclusion arrived at by the local planning authorities pursuant to those EIA Directive articles.

In determining the Application we have considered the following documents: -

- The Environmental Statement submitted with the planning application (which also formed part of the Environmental Permit Application).
- The decision of Wirral Borough Council to grant planning permission on 25/09/14.
- The report and decision notice of the local planning authority accompanying the grant of planning permission.
- The response of the Environment Agency to the local planning authority in its role as consultee to the planning process.

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From consideration of all the documents above, the Environment Agency considers that no additional or different conditions are necessary.

The Environment Agency has also carried out its own consultation on the Environmental Permitting Application which includes the Environmental Statement submitted to the local planning authority. The results of our consultation are described elsewhere in this decision document.

7.1.2 Schedule 9 to the EPR 2010 – Waste Framework Directive

As the Installation involves the treatment of waste, it is carrying out a *waste* operation for the purposes of the EPR 2010, and the requirements of Schedule 9 therefore apply. This means that we must exercise our functions so as to ensure implementation of certain articles of the WFD.

We must exercise our relevant functions for the purposes of ensuring that the waste hierarchy referred to in Article 4 of the Waste Framework Directive is applied to the generation of waste and that any waste generated is treated in accordance with Article 4 of the Waste Framework Directive. (See also section 4.3.9)

The conditions of the permit ensure that waste generation from the facility is minimised. Where the production of waste cannot be prevented it will be recovered wherever possible or otherwise disposed of in a manner that minimises its impact on the environment. This is in accordance with Article 4.

We must also exercise our relevant functions for the purposes of implementing Article 13 of the Waste Framework Directive; ensuring that the requirements in the second paragraph of Article 23(1) of the Waste Framework Directive are met; and ensuring compliance with Articles 18(2)(b), 18(2)(c), 23(3), 23(4) and 35(1) of the Waste Framework Directive.

Article 13 relates to the protection of human health and the environment. These objectives are addressed elsewhere in this document.

Article 23(1) requires the permit to specify:

- (a) the types and quantities of waste that may be treated;
- (b) for each type of operation permitted, the technical and any other requirements relevant to the site concerned:
- (c) the safety and precautionary measures to be taken;
- (d) the method to be used for each type of operation;
- (e) such monitoring and control operations as may be necessary;
- (f) such closure and after-care provisions as may be necessary.

These are all covered by permit conditions.

The permit does not allow the mixing of hazardous waste so Article 18(2) is not relevant.

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We consider that the intended method of waste treatment is acceptable from the point of view of environmental protection so Article 23(3) does not apply. Energy efficiency is dealt with elsewhere in this document but we consider the conditions of the permit ensure that the recovery of energy take place with a high level of energy efficiency in accordance with Article 23(4).

Article 35(1) relates to record keeping and its requirements are delivered through permit conditions.

7.1.3 Schedule 22 to the EPR 2010 – Groundwater, Water Framework and Groundwater Daughter Directives

To the extent that it might lead to a discharge of pollutants to groundwater (a "groundwater activity" under the EPR 2010), the Permit is subject to the requirements of Schedule 22, which delivers the requirements of EU Directives relating to pollution of groundwater. The Permit will require the taking of all necessary measures to prevent the input of any hazardous substances to groundwater, and to limit the input of non-hazardous pollutants into groundwater so as to ensure such pollutants do not cause pollution, and satisfies the requirements of Schedule 22.

No releases to groundwater from the Installation are permitted. The Permit also requires material storage areas to be designed and maintained to a high standard to prevent accidental releases.

7.1.4 Directive 2003/35/EC – The Public Participation Directive

Regulation 59 of the EPR 2010 requires the Environment Agency to prepare and publish a statement of its policies for complying with its public participation duties. We have published our public participation statement.

This Application has been consulted upon in line with this statement. This satisfies the requirements of the Public Participation Directive.

7.2 <u>National primary legislation</u>

7.2.1 Environment Act 1995

(i) Section 4 (Pursuit of Sustainable Development)

We are required to contribute towards achieving sustainable development, as considered appropriate by Ministers and set out in guidance issued to us. The Secretary of State for Environment, Food and Rural Affairs has issued *The Environment Agency's Objectives and Contribution to Sustainable Development: Statutory Guidance (December 2002)*. This document:

"provides guidance to the Agency on such matters as the formulation of approaches that the Agency should take to its work, decisions about priorities for the Agency and the allocation of resources. It is not directly applicable to individual regulatory decisions of the Agency".

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In respect of regulation of industrial pollution through the EPR, the Guidance refers in particular to the objective of setting permit conditions "in a consistent and proportionate fashion based on Best Available Techniques and taking into account all relevant matters...". The Environment Agency considers that it has pursued the objectives set out in the Government's guidance, where relevant, and that there are no additional conditions that should be included in this Permit to take account of the Section 4 duty.

(ii) Section 7 (Pursuit of Conservation Objectives)

We considered whether we should impose any additional or different requirements in terms of our duty to have regard to the various conservation objectives set out in Section 7, but concluded that we should not.

We have considered the impact of the installation on local wildlife sites within 2Km which are not designated as either European Sites or SSSIs. We are satisfied that no additional conditions are required.

(iii) Section 81 (National Air Quality Strategy)

We have had regard to the National Air Quality Strategy and consider that our decision complies with the Strategy, and that no additional or different conditions are appropriate for this Permit.

7.2.2 Human Rights Act 1998

We have considered potential interference with rights addressed by the European Convention on Human Rights in reaching our decision and consider that our decision is compatible with our duties under the Human Rights Act 1998. In particular, we have considered the right to life (Article 2), the right to a fair trial (Article 6), the right to respect for private and family life (Article 8) and the right to protection of property (Article 1, First Protocol). We do not believe that Convention rights are engaged in relation to this determination.

7.2.3 Countryside and Rights of Way Act 2000 (CROW 2000)

Section 85 of this Act imposes a duty on Environment Agency to have regard to the purpose of conserving and enhancing the natural beauty of the area of outstanding natural beauty (AONB). There is no AONB which could be affected by the Installation.

7.2.4 Wildlife and Countryside Act 1981

Under section 28G of the Wildlife and Countryside Act 1981 the Environment Agency has a duty to take reasonable steps to further the conservation and enhancement of the flora, fauna or geological or physiographical features by reason of which a site is of special scientific interest. Under section 28I the Environment Agency has a duty to consult Natural England in relation to any permit that is likely to damage SSSIs.

We assessed the Application and concluded that the Installation will not damage the special features of any SSSI. This was recorded on a CROW Appendix 4 form.

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The CROW assessment is summarised in greater detail in section 5.4.3 of this document. A copy of the full Appendix 4 Assessment can be found on the public register.

7.2.5 Natural Environment and Rural Communities Act 2006

Section 40 of this Act requires us to have regard, so far as is consistent with the proper exercise of our functions, to the purpose of conserving biodiversity. We have done so and consider that no different or additional conditions in the Permit are required.

7.3 National secondary legislation

7.3.1 The Conservation of Natural Habitats and Species Regulations 2010

We have assessed the Application in accordance with guidance agreed jointly with Natural England / CCW and concluded that there will be no likely significant effect on any European Site.

We consulted Natural England / CCW by means of an Appendix 11 assessment, and they considered that the operation of the Installation would not have a likely significant effect on the interest features of protected sites.

The habitat assessment is summarised in greater detail in section 5.4 of this document. A copy of the full Appendix 11 Assessment can be found on the public register.

7.3.2 Water Framework Directive Regulations 2003

Consideration has been given to whether any additional requirements should be imposed in terms of the Environment Agency's duty under regulation 3 to secure the requirements of the Water Framework Directive through (inter alia) EP permits, but it is felt that existing conditions are sufficient in this regard and no other appropriate requirements have been identified.

7.3.3 The Persistent Organic Pollutants Regulations 2007

We have explained our approach to these Regulations, which give effect to the Stockholm Convention on POPs and the EU's POPs Regulation, above.

7.4 Other relevant legal requirements

7.4.1 Duty to Involve

S23 of the Local Democracy, Economic Development and Construction Act 2009 require us where we consider it appropriate to take such steps as we consider appropriate to secure the involvement of interested persons in the exercise of our functions by providing them with information, consulting them

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or involving them in any other way. S24 requires us to have regard to any Secretary of State guidance as to how we should do that.

The way in which the Environment Agency has consulted with the public and other interested parties is set out in section 2.2 of this document. The way in which we have taken account of the representations we have received is set out in Annex 4. Our public consultation duties are also set out in the EP Regulations, and our statutory Public Participation Statement, which implement the requirements of the Public Participation Directive.

ANNEX 1: APPLICATION OF CHAPTER IV OF THE INDUSTRIAL EMISSIONS DIRECTIVE

IED Article	Requirement	Delivered by
45(1)(a)	The permit shall include a list of all types of waste which may be treated using at least the types of waste set out in the European Waste List established by Decision 2000/532/EC, if possible, and containing information on the quantity of each type of waste, where appropriate.	Condition 2.3.3(a) and Table S2.2 in Schedule 2 of the Permit.
45(1)(b)	The permit shall include the total waste incinerating or co-incinerating capacity of the plant.	Condition 2.3.3(a) and Table S2.2 in Schedule 2 of the Permit.
45(1)(c)	The permit shall include the limit values for emissions into air and water.	Conditions 3.1.1 and 3.1.2 and Tables S3.1, S3.1(a), S3.2 and S3.3 in Schedule 3 of the Permit.
45(1)(d)	The permit shall include the requirements for pH, temperature and flow of waste water discharges.	Not Applicable
45(1)(e)	The permit shall include the sampling and measurement procedures and frequencies to be used to comply with the conditions set for emissions monitoring.	Conditions 3.5.1 to 3.5.5 and Tables S3.1, S3.1(a), S3.2, S3.3 and S3.4 in Schedule 3 of the Permit.
45(1)(f)	The permit shall include the maximum permissible period of unavoidable stoppages, disturbances or failures of the purification devices or the measurement devices, during which the emissions into the air and the discharges of waste water may exceed the prescribed emission limit values.	Conditions 2.3.10 and 2.3.11.
45(2)(a)	The permit shall include a list of the quantities of the different categories of hazardous waste which may be treated.	Not Applicable
45(2)(b)	The permit shall include the	Not Applicable

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IED Article	Requirement	Delivered by
	minimum and maximum mass flows of those hazardous waste, their lowest and maximum calorific values and the maximum contents of polychlorinated biphenyls, pentachlorophenol, chlorine, fluorine, sulphur, heavy metals and other polluting substances.	
46(1)	Waste gases shall be discharged in a controlled way by means of a stack the height of which is calculated in such a way as to safeguard human health and the environment.	Condition 2.3.1(a) and Table S1.2 of Schedule 1 of the Permit.
46(2)	Emission into air shall not exceed the emission limit values set out in part of Annex VI.	Conditions 3.1.1 and 3.1.2 and Tables S3.1 and S3.1a.
46(2)	Emission into air shall not exceed the emission limit values set out in parts 4 or determined in accordance with part 4 of Annex VI.	Conditions 3.1.1 and 3.1.2 and Tables S3.1 and S3.1a.
46(3)	Relates to conditions for water discharges from the cleaning of exhaust gases.	There are no such discharges as condition 3.1.1 prohibits this.
46(4)	Relates to conditions for water discharges from the cleaning of exhaust gases.	There are no such discharges as condition 3.1.1 prohibits this.
46(5)	Prevention of unauthorised and accidental release of any polluting substances into soil, surface water or groundwater. Adequate storage capacity for contaminated rainwater run-off from the site or for contaminated water from spillage or fire-fighting.	The application explains the measures to be in place for achieving the directive requirements
46(6)	Limits the maximum period of operation when an ELV is exceeded to 4 hours uninterrupted duration in any one instance, and with a maximum cumulative limit of 60 hours per year. Limits on dust (150 mg/m³), CO and	Conditions 2.3.10 and 2.3.11

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IED Article	Requirement	Delivered by
	TOC not to be exceeded during this	
	period.	
47	In the event of breakdown, reduce or close down operations as soon as practicable. Limits on dust (150 mg/m³), CO and TOC not to be exceeded during this period.	Condition 2.3.10
48(1)	Monitoring of emissions is carried out in accordance with Parts 6 and 7 of Annex VI.	Conditions 3.5.1 to 3.5.5. Reference conditions are defined in Schedule 6 of the Permit.
48(2)	Installation and functioning of the automated measurement systems shall be subject to control and to annual surveillance tests as set out in point 1 of Part 6 of Annex VI.	Condition 3.5.3, and tables S3.1, S3.1(a), and S3.4
48(3)	The competent authority shall determine the location of sampling or measurement points to be used for monitoring of emissions.	Conditions 3.5.3 and 3.5.4
48(4)	All monitoring results shall be recorded, processed and presented in such a way as to enable the competent authority to verify compliance with the operating conditions and emission limit values which are included in the permit.	Conditions 4.1.1 and 4.1.2, and Tables S4.1 and S4.4
49	The emission limit values for air and water shall be regarded as being complied with if the conditions described in Part 8 of Annex VI are fulfilled.	Conditions 3.1.1 and 3.1.2
50(1)	Slag and bottom ash to have Total Organic Carbon (TOC) < 3% or loss on ignition (LOI) < 5%.	Conditions 3.5.1 and Table S3.5
50(2)	Flue gas to be raised to a temperature of 850°C for two seconds, as measured at representative point of the combustion chamber.	Condition 2.3.9, Pre- operational condition PO5 and Improvement condition IC3.
50(3)	At least one auxiliary burner which must not be fed with fuels which can cause higher emissions than those resulting from the burning of gas oil liquefied gas or natural gas.	Condition 2.3.7

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IED Article	Requirement	Delivered by
50(4)(a)	Automatic shut to prevent waste feed if at start up until the specified temperature has been reached.	Condition 2.3.6
50(4)(b)	Automatic shut to prevent waste feed if the combustion temperature is not maintained.	Condition 2.3.6
50(4)(c)	Automatic shut to prevent waste feed if the CEMs show that ELVs are exceeded due to disturbances or failure of waste cleaning devices.	Condition 2.3.6
50(5)	Any heat generated from the process shall be recovered as far as practicable.	(a) The plant will generate electricity (b)Operator to review the available heat recovery options prior to commissioning (Condition PO1) and then every 2 years (Conditions 1.2. 1 to 1.2.3)
50(6)	Relates to the feeding of infectious clinical waste into the furnace.	No infectious clinical waste will be burnt
50(7)	Management of the Installation to be in the hands of a natural person who is competent to manage it.	Conditions 1.1.1 to 1.1.3.
51(1)	Different conditions than those laid down in Article 50(1), (2) and (3) and, as regards the temperature Article 50(4) may be authorised, provided the other requirements of this chapter are me.	No such conditions have been allowed
51(2)	Changes in operating conditions do not cause more residues or residues with a higher content of organic polluting substances compared to those residues which could be expected under the conditions laid down in Articles 50(1), (2) and (3).	No such conditions have been allowed
51(3)	Changes in operating conditions shall include emission limit values for CO and TOC set out in Part 3 of Annex VI.	No such conditions have been allowed
52(1)	Take all necessary precautions concerning delivery and reception of Wastes, to prevent or minimise pollution.	Conditions 2.3.1, 2.3.3, 3.2, 3.3, 3.4 and 3.6.

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IED Article	Requirement	Delivered by
52(2)	Determine the mass of each category of wastes, if possible according to the EWC, prior to accepting the waste.	Condition 2.3.3(a) and Table S2.2 in Schedule 3 of the Permit.
52(3)	Prior to accepting hazardous waste, the operator shall collect available information about the waste for the purpose of compliance with the permit requirements specified in Article 45(2).	Not Applicable
52(4)	Prior to accepting hazardous waste, the operator shall carry out the procedures set out in Article 52(4).	Not Applicable
52(5)	Granting of exemptions from Article 52(2), (3) and (4).	Not Applicable
53(1)	Residues to be minimised in their amount and harmfulness, and recycled where appropriate.	Conditions 1.4.1, 1.4.2 and 3.5.1 with Table S3.5
53(2)	Prevent dispersal of dry residues and dust during transport and storage.	Conditions 1.4.1 2.3.1(a) and 3.2.1.
53(3)	Test residues for their physical and chemical characteristics and polluting potential including heavy metal content (soluble fraction).	Condition 3.5.1 and Table S3.5 and pre- operational condition PO2.
55(1)	Application, decision and permit to be publicly available.	All documents are accessible from the Environment Agency Public Register.
55(2)	An annual report on plant operation and monitoring for all plants burning more than 2 tonne/hour waste.	Condition 4.2.2 and 4.2.3.

ANNEX 2: Pre-Operational Conditions

Based on the information on the Application, we consider that we do need to impose pre-operational conditions. These conditions are set out below and referred to, where applicable, in the text of the decision document. We are using these conditions to require the Operator to confirm that the details and measures proposed in the Application have been adopted or implemented prior to the operation of the Installation.

Reference	Pre-operational measures
PO1	Prior to the commencement of commissioning, the Operator shall send a report to the Environment Agency which will contain a comprehensive review of the options available for utilising the heat generated by the waste incineration process in order to ensure that it is recovered as far as practicable. The review shall detail any identified proposals for improving the recovery and utilisation of waste heat and shall provide a timetable for their implementation.
PO2	Prior to the commencement of commissioning, the Operator shall submit to the Environment Agency for approval a protocol for the sampling and testing of incinerator bottom ash for the purposes of assessing its hazard status. Sampling and testing shall be carried out in accordance with the protocol as approved.
PO3	At least 2 months prior to the commencement of commissioning; the Operator shall provide a written commissioning plan, including timelines for completion, for approval by the Environment Agency. The commissioning plan shall include the expected emissions to the environment during the different stages of commissioning, the expected durations of commissioning activities and the actions to be taken to protect the environment and report to the Environment Agency in the event that actual emissions exceed expected emissions. Commissioning shall be carried out in accordance with the commissioning plan as approved.
PO4	At least 2 month prior to the commencement of commissioning, the Operator shall submit a written report to the Agency detailing the waste acceptance procedure to be used at the site. The waste acceptance procedure shall include the process and systems by which wastes unsuitable for incineration at the site will be controlled. The procedure shall be implemented in accordance with the written approval from the Agency.
PO5	After completion of furnace design and at least three calendar months before any furnace operation; the operator shall submit a written report to the Agency of the details of the computational fluid dynamic (CFD) modelling. The report shall demonstrate whether the design combustion conditions comply with the residence time and temperature requirements as defined by the Industrial Emissions Directive.
PO6	Prior to the commencement of commissioning, the operator shall submit a written report to the Agency for approval that includes 'as built' detailed site drainage plans (internal process water) and the specific design detail of the external surface water drainage systems and containment infrastructure at the site, including all sub-surface structures and equipment. The report shall also include an inspection and maintenance programmes for the containment infrastructure and equipment at the site.
P07	Prior to the commencement of commissioning the Operator shall submit the written protocol referenced in condition 3.2.4 for the monitoring of soil and groundwater for approval by the Environment Agency. The protocol shall demonstrate how the Operator will meet the requirements of Articles 14(1)(b),

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	14(1)(e) and 16(2) of the IED.
PO8	The Operator shall prepare and submit to the Environment Agency for approval an Odour Management Plan with regard to the requirements set out in the Agency's Horizontal Guidance Note H4 (Odour management). In particular the Odour Management Plan shall review odour control measures/ equipment/ procedures associated with the operation of the Installation; and propose additional measures/ equipment/ procedures as necessary to control remaining odours with a timescale for implementation.
PO9	The Operator shall develop and implement formal documented procedures for the preventative inspection and subsequent maintenance of all process items that pose a potential nuisance risk through odour. These procedures shall also include documented procedures for the preventative inspection and maintenance of all items of infrastructure that have been installed to mitigate the potential odour impacts posed by the installation. The Operator shall provide the Agency with a written copy of these procedures.
PO10	At least 2 months prior to the commencement of commissioning, the Operator shall submit to the Environment Agency for approval the final design for the fuel storage area and procedures for the removal of unacceptable waste.
PO11	Prior to the commencement of commissioning, the operator shall submit a written report to the Agency for approval an assessment of environmental hazards in the event of failure of pollution prevention measures including but not limited to ventilation failures, door failures, equipment leakage and failure of abatement measures.

ANNEX 3: Improvement Conditions

Based in the information in the Application we consider that we need to set improvement conditions. These conditions are set out below - justifications for these are provided at the relevant section of the decision document. We are using these conditions to require the Operator to provide the Environment Agency with details that need to be established or confirmed during and/or after commissioning.

Reference	Improvement measure	Completion date
IC1	The Operator shall submit a written report to the Environment Agency on the implementation of its Environmental Management System and the progress made in the certification of the system by an external body or if appropriate submit a schedule by which the EMS will be certified.	Within 12 months of the date on which waste is first burnt.
IC2	The Operator shall submit a written report to the Environment Agency on the commissioning of the installation. The report shall summarise the environmental performance of the plant as installed against the design parameters set out in the Application. The report shall also include a review of the performance of the facility against the conditions of this permit and details of procedures developed during commissioning for achieving and demonstrating compliance with permit conditions.	Within 4 months of the completion of commissioning.
IC3	The Operator shall carry out checks to verify the residence time, minimum temperature and oxygen content of the exhaust gases in the furnace whilst operating under the anticipated most unfavourable operating conditions. The results shall be submitted in writing to the Environment Agency.	Within 4 months of the completion of commissioning.
IC4	The Operator shall submit a written report to the Environment Agency describing the performance and optimisation of the Selective Catalytic Reduction (SCR) system and combustion settings to minimise oxides of nitrogen (NO _x) emissions within the emission limit values described in this permit with the minimisation of nitrous oxide emissions. The report shall include an assessment of the level of NO _x and N ₂ O emissions that can be achieved under optimum operating conditions. The report shall also provide details of the optimisation (including dosing rates) for the control of acid gases and dioxins	Within 4 months of the completion of commissioning.

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IC5	The Operator shall carry out an assessment of the impact of emissions to air of the following component metals subject to emission limit values, cadmium, lead, manganese, vanadium, nickel, arsenic and chromium (VI). A report on the assessment shall be made to the Environment Agency.	15 months from commencement of operations
	Emissions monitoring data obtained during the first year of operation shall be used to compare the actual emissions with those assumed in the impact assessment submitted with the Application. An assessment shall be made of the impact of each metal against the relevant EQS/EAL. In the event that the assessment shows that an EQS/EAL can be exceeded, the report shall include proposals for further investigative work.	
IC6	The Operator shall submit a written summary report to the Agency to confirm by the results of calibration and verification testing that the performance of Continuous Emission Monitors for parameters as specified in Table S3.1 and Table S3.1(a) complies with the requirements of BS EN 14181, specifically the requirements of QAL1, QAL2 and QAL3.	Initial calibration report to be submitted to the Agency within 3 months of completion of commissioning. Full summary evidence compliance report to be submitted within 18 months of commissioning.

ANNEX 4: Consultation Reponses

A) Advertising and Consultation on the Application

The Application has been advertised and consulted upon in accordance with the Environment Agency's Public Participation Statement. The way in which this has been carried out along with the results of our consultation and how we have taken consultation responses into account in reaching our draft decision is summarised in this Annex. Copies of all consultation responses have been placed on the Environment Agency and Local Authority public registers.

The Application was advertised on the Environment Agency website from 21/08/14 to 19/09/14.

The Application was re-advertised on the Environment Agency website from 24/09/15 to 23/10/15 in line with our procedures due to a change in operator.

The following statutory and non-statutory bodies were consulted: -

- Public Health England (PHE)
- Wirral Metropolitan Borough Council (NHS) Director of Public Health
- Wirral Metropolitan Borough Council Planning Department
- Wirral Metropolitan Borough Council Environmental Protection Department
- Health and Safety Executive (HSE)
- Food Standards Agency (FSA)
- Sewerage Undertaker United Utilities

1) Consultation Responses from Statutory and Non-Statutory Bodies

Response Received from Natural England		
Brief summary of issues raised:	Summary of action taken / how this has been covered	

Response Received from Public Health England		
Brief summary of issues raised:	Summary of action taken / how this	
	has been covered	
The human health risk assessment concluded that emissions to air from the proposed facility will not pose unacceptable health risks to the residential, farmer or fisher locations identified in the vicinity of the proposed facility.	No further action required.	
This response is based on the assumption that the permit holder		

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shall take all appropriate measures to prevent or control pollution, in accordance with the relevant sector guidance, industry best practice and guidance for preventing and responding to fires given the industrial location of the proposed site. The PHE (formally HPA) has issued an updated position statement on Municipal Solid Waste Incineration that states: "The Health Protection Agency has reviewed research undertaken to examine the suggested links between emissions from municipal waste incinerators and effects on health. While it is not possible to rule out adverse health effects from modern, well regulated municipal waste incinerators with complete certainty, any potential damage to the health of those living close- by is likely to be very small, if detectable. This view is based on detailed assessments of the effects of air pollutants on health and on the fact that modern and well managed municipal waste incinerators make only a very small contribution to local concentrations of air pollutants."

Response Received from Wirral Metropolitan Borough Council - Regeneration & Environment Directorate

Brief summary of issues raised:

Bearing in mind the proximity of the nearest dwelling (approx 700m from buildings containing plant) it is felt that the proposals for noise control measures contained in the applicants Environmental Statement (section 10 of Volume 2 paras 10.6.3 & 10.6.4 in their latest planning application should be reflected in permit conditions wherever it is practicable to do so.

There is limited discussion of odour control measures within the proposals

Summary of action taken / how this has been covered

Our assessment of noise control and emissions from the Installation is recorded at Section 6.5.5 of this document and we are satisfied that suitable noise controls will be in place and that there will be no significant impact on noise associated with normal operation. However standard Permit condition 3.4 addresses any potential issues with noise or vibration.

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and it may be prudent to include this
in the conditions.

Response Received from Wirral Metropolitan Borough Council - Planning Department Summary of action taken / how this Brief summary of issues raised: has been covered The modelling study and our The Planning Committee stated that the 'stack' is considerably higher than assessment of impact from the that previously proposed. They Installation is based on the ELV's now expected that the minimal output included in the permit, and therefore of gases should be dispersed by compliance with those monitored these means and by abatement. limits will ensure that impacts are within the values predicted in the Whilst they expected that the plant impact assessment. should be in continuous operation. and not taken out of operation, they In addition we considered the impact had some concern that the shut down of abnormal emissions in section 5.5 / start up conditions appear to be a and concluded that all emissions source of potential local pollution as have been assessed as being unlikely the gases may not be 'forced up' as to give rise to significant pollution. expected and underlined concerns regarding temperature inversion.

Response Received from United Utilities		
Brief summary of issues raised:	Summary of action taken / how this has been covered	
United Utilities were aware that an application for a Trade Effluent Consent will be forthcoming.		

Response Received from the Health and Safety Executive		
Brief summary of issues raised:	Summary of action taken / how this	
	has been covered	
No comments were made concerning	-	
the application.		

Response Received from the Food Standards Agency		
Brief summary of issues raised:	Summary of action taken / how this has been covered	
No response received	-	

Response Received from Natural Resources Wales		
Brief summary of issues raised:	Summary of action taken / how this has been covered	
No response received	-	

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2) <u>Consultation Responses from Members of the Public and Community Organisations</u>

No responses were received.

a) Representations from Local MP, Councillors and Parish / Town / Community Councils

Representations were received from Councillor Phil Gilchrist, who raised the issues detailed in the response from the Planning Committee detailed above.

b) Representations from Community and Other Organisations

No responses were received.

c) Representations from Individual Members of the Public

No responses were received.

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